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# <sup>1</sup> **CO<sup>2</sup> Solubility in Kimberlite melts**

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### 11 **ABSTRACT**

12 Carbon dioxide is the most abundant volatile in kimberlite melts and its solubility exerts a 13 prime influence on the melt structure, buoyancy, transport rate and hence eruption dynamics. 14 The actual primary composition of kimberlite magma is the matter of some debate but the 15 solubility of  $CO<sub>2</sub>$  in kimberlitic melts is also poorly constrained due to difficulties in 16 quenching these compositions to a glass that retains the equilibrium  $CO<sub>2</sub>$  content. In this 17 study we used a range of synthetic, melt compositions with broadly kimberlitic to carbonatitic 18 characteristics which can, under certain conditions, be quenched fast enough to produce a 19 glass. These materials are used to determine the  $CO<sub>2</sub>$  solubility as a function of chemical 20 composition and pressure (0.05-1.5 GPa). Our results suggest that the solubility of  $CO<sub>2</sub>$ 21 decreases steadily with increasing amount of network forming cations from  $\sim$ 30 wt% CO<sub>2</sub> at 22 12 wt% SiO<sub>2</sub> down to ~3 wt% CO<sub>2</sub> at 40 wt% SiO<sub>2</sub>. For low silica melts, CO<sub>2</sub> solubility 23 correlates non-linearly with pressure showing a sudden increase from 0.1 to 100 MPa and a 24 smooth increase for pressure >100 MPa. This peculiar pressure-solubility relationship in low 25 silica melts implies that  $CO<sub>2</sub>$  degassing must mostly occur within the last 3 km of ascent to 26 the surface having potential links with the highly explosive nature of kimberlite magmas and 27 some of the geo-morphological features of their root zone. We present an empirical  $CO<sub>2</sub>$ 28 solubility model covering a large range of melt composition from 11 to 55 wt%  $SiO<sub>2</sub>$ 29 spanning the transition from carbonatitic to kimberlitic at pressures from 1500 to 50 MPa. 30 Keywords: kimberlite; carbonatite;  $CO<sub>2</sub>$  solubility; transitional melt

# 31 **1. INTRODUCTION**

32 Experimental investigation of the solubility of  $CO<sub>2</sub>$  in kimberlite melt has been limited due to the difficulty in quenching such melt fast enough to form a pure glass (e.g. Brey and 34 Ryabchikov, 1994). Previous studies have therefore estimated the  $CO_2$  solubility based on: (i) extrapolation from trend defined in silicate melts (Brooker et al., 2001) (ii) solubility of melt in partially to highly crystallised experiments (Brooker et al., 2011) (iii) solubility at 0.1 MPa of simple, four components, synthetic compositions considered as analogue to the natural system (Russell et al., 2012) (iv) molecular dynamics simulation studies (Guillot and Sator, 2011). While these studies all suggest that the solubility of  $CO<sub>2</sub>$  decreases as the melt becomes enriched in silica, the effect of pressure has remained speculative. Our current 41 knowledge from experimental studies on silicate melt suggests that  $CO<sub>2</sub>$  solubility increases with pressure (Blank and Brooker, 1994; Iacono-Marziano et al., 2012; Morizet et al., 2002, 43 2014) while in pure carbonate melts,  $CO<sub>2</sub>$  solubility is more related to satisfying stoichiometric requirements and therefore less dependent on pressure as exemplified by Oldoinyo Lengai's alkali carbonatite lava (Kervyn et al., 2008). However, experiments from 46 Wyllie (1989) and Brooker & Kjardgaard (2011) suggest that there is some 'excess'  $CO<sub>2</sub>$ 47 solubility in pure  $CaCO<sub>3</sub>$  melt, apparently causing a decrease in liquidus temperature.

48 The composition of primary kimberlite melts in term of volatile and major element chemistry 49 is poorly constrained. Not only are natural kimberlite laden with xenolith and xenocryst

 (Mitchell, 2008), but the strong alteration by external fluids they typically endured, in particular serpentinization, strongly affects the volatile and major element composition (Brooker et al., 2011; Sparks et al., 2009). Latest attempt to back-calculate the kimberlite melts chemistry by removal of the serpentinization process points towards an original melt 54 being richer in  $CO_2$  and  $CaO$  and poorer in  $SiO_2$ , water and MgO than calculated from "uncontaminated" kimberlites (Brooker et al., 2011; Sparks et al., 2009). This findings are corroborated with the fact that the Mg number in kimberlite is too high for equilibrium with a mantle sources (Kopylova et al., 2007; Price et al., 2000) and that liquidus temperature for "uncontaminated" kimberlite composition of 1400°C (Brooker et al., 2011) are higher than predicted from mineral thermometry (Fedortchouk et al., 2002). We therefore chose here to follow from the work of Brooker et al (2011) who argued that kimberlite melts are originally transitional, that is, they have a composition intermediate between a carbonate and a silicate 62 liquid, and investigated several melt compositions with  $SiO<sub>2</sub>$  contents between 11 and 32 wt%.

 In this contribution, we present results on the first experimental kimberlitic glasses synthesised using an internally heated pressure vessel (IHPV) equipped with an optimised quench configuration. We produced a series of melt compositions across the "transitional" 68 melt field (SiO<sub>2</sub> ~18 to ~32 wt%) to assess the effect of silica activity on  $CO_2$  solubility. The effect of pressure was then investigated by equilibrating melts of similar composition at different pressures (50 to 1500 MPa).

## **2. EXPERIMENTAL METHODOLOGY**

#### **2.1 Starting material**

 Starting materials were produced by mixing powders from a natural lamproite from Torre Alfina, Italy ( table 1, see Peccerillo et al., 1988) with various amounts of synthetic powders of pure oxides and natural dolomite. In order to ensure homogeneity and remove the volatiles present in the Torre Alfina rock, it was fused twice in air at 1400°C and quenched to glass. The composition of all mixtures used as starting materials of all experiments is reported in table 1. The melt compositions we have synthesized here are very Ca-rich when compared to the more Mg-rich typical "contamination free" kimberlite (Mitchell, 1986) but later compare our findings to experiments with more Mg-rich composition. Therefore, an underlying supposition of our work is that Mg and Ca cations behave in a similar way with respect to CO<sup>2</sup> solubility in the melt (see Brey et al., 1991 and Brey and Ryabchikov, 1994 for an 84 investigation of the effect of Mg-Ca substitution on  $CO<sub>2</sub>$  solubility in kimberlite melts and see discussion section 5). The Al content of the composition presented here might also be considered slightly high by some authors while the Fe content would be considered low. Notwithstanding these differences, the compositions we explored here provide a close analogue to kimberlite melts (in term of NBO/T for instance) for which the true composition remains unknown and debated (see review by Sparks 2013).

# **2.2 High pressure experiments; internally heated pressure vessels and piston cylinder**

93 To investigate the solubility of  $CO<sub>2</sub>$  in transitional melts at crustal pressure, we performed a series of solubility experiments in the pressure range 50 to 350 MPa at relatively constant 95 temperature (1225 to 1270<sup>o</sup>C) in relatively dry and oxidized conditions ( $logfO<sub>2</sub>= FMQ+3$ ).

 We used internally heated pressure vessels at the ISTO-CNRS laboratory in Orléans, which 97 can reach pressures of up to 400 MPa ( $\pm$  3 MPa) under controlled temperature up to 1300 °C 98 ( $\pm$  2°C). The vessel was pressurised using argon gas as the pressure medium. A two-Mo-99 winding vertical furnace was used, creating a 5cm isothermal  $(\pm 5^{\circ}C)$  "hot-spot" zone and controlled by two S-type thermocouples located on both side of the sample.

 Experimental charges consisted of anhydrous sample powder (30 to 150 mg) loaded in gold-102 palladium ( $\text{Au}_{80} \text{Pd}_{20}$ ) or platinum capsules (2 to 4 cm in length, 2.5 mm inner diameter and 2.9 mm outer diameter). The capsules were welded shut. Although the initial powder mixtures were stored at 120°C, the strongly hydroscopic character of some oxides (in 105 particular MgO, NaO and K<sub>2</sub>O) absorbing atmospheric H<sub>2</sub>O within the 15 min necessary to load the capsules, made it impossible to obtain fully water-free experimental charges, hence 107 lowering slightly the  $XCO<sub>2</sub>$  in the fluid in equilibrium with the melt at P & T. For each experiment, one to three capsules were hanged by a thin Pt wire. The temperature gradient 109 along the "hot-spot" zone, where the capsules were located, was maintained at about  $10^{\circ}$ C; the hot zone was always on the top end of the sample. This gradient, although inducing an uncertainty in the run temperature, was part of the quench optimisation strategy as it imposed a thermal profile in the furnace that ensures a strong thermal contrast over a small vertical length located directly below the hanged capsule. Rapid quenching was achieved by passing an electrical current to the holding Pt wire so that the sample dropped into the cold, bottom 115 part of the furnace. The cooling rate was estimated to >100-200 $^{\circ}$ C s<sup>-1</sup> although no precise estimate could be obtained. After each experiment, capsules were weighed (i) before and (ii) after, opening in order to (i) verify that no leakage had occurred, and (ii) determine the amount of gas not incorporated in the glass. Capsules were then opened and a fragment of the charge was embedded in an epoxy resin and polished for SEM and microprobe analyses. We conducted a total of 18 solubility experiments. The strategy was first to produce a complete

121 isobaric section at 350 MPa, for a range of melt chemistry spanning  $SiO<sub>2</sub>$  from 11 to 38 wt% (expressed as nominal starting composition, Table 1). We then explored the effect of pressure 123 on several compositions (between 17 and 38 wt%  $SiO<sub>2</sub>$ ; expressed as nominal starting composition) from 50 to 350 MPa at temperatures of 1225 to 1270°C. While most experiments successfully produced a pure glass (Fig. 1 and Fig.S1), experiments performed at 126 50 MPa (run number: TA6\_1\_6 and TA7\_1\_3), one experiment at 100 MPa (run number: 127 TA10\_1\_2) and the experiment with lowest  $SiO<sub>2</sub>$  (run number TA15\_1\_1) could not be quenched fast enough and quench crystals were present throughout the experimental charge (these crystals could not be analysed free of the glass component).

 A single piston cylinder experiment was performed at 1.5 GPa and 1300°C in a ½ inch piston-cylinder apparatus. Experimental charge consisted of natural anhydrous sample 133 powder (30 mg) loaded in gold-palladium ( $Au_{80}Pd_{20}$ ) capsules (1 cm in length, 2.5 mm inner diameter and 2.9 mm outer diameter). The capsule was introduced in a talc–pyrex–graphite 135 furnace assembly and surrounded by MgO. A B-type thermocouple was located at  $\sim$ 1 mm atop of the capsule and the run temperature should be considered as a minimum value. The quench of the piston cylinder assembly was not fast enough to prevent the pervasive growth of quench crystals (Fig. 1; Fig. S1; experiment TA6\_1\_5).

**3. ANALYTICAL TECHNIQUES** 

#### **3.1 EMPA**

 All experimental products were examined by optical microscope and scanning electronic microscope (SEM) to check for the presence of quench crystals (Fig. S1). Electron microprobe analyses (EMPA) were performed on a Cameca SXFive at the ISTO-CNRS laboratory in Orléans. Glasses were analysed using an accelerating voltage of 15 kV, a beam

 current of 6 nA and a defocused beam of 10 µm. Na and K were analysed first in order to minimise alkali loss during analysis. The shortfall in the totals for analysed glasses was 147 broadly consistent with the  $CO<sub>2</sub>$  content estimated by other techniques, but systematically higher (Fig. S2).

#### **3.2 Micro-Raman**

 We used an Innova 300-5W Argon ion laser (Coherent©) operating at 514 nm as the light source to produce Raman scattering. Spectra were collected by a Jobin-Yvon Labram spectrometer (focal distance = 300 mm) equipped with a 2400 grooves/mm CCD detector. Analyses were performed in confocal mode (hole= 500 μm, slit = 200μm) and using a x50 155 . Olympus objective reducing the analysed volume size to a few  $\mu$ m<sup>3</sup>. Spectra were acquired 156 over the aluminosilicate network and  $CO_3^2$  region between 200 and 1350 cm<sup>-1</sup>. In a few cases 157 spectra were also acquired in the OH region between 2500 and 3900 cm<sup>-1</sup>. The acquisition time was of 10 x 60 sec and acquisition depth was optimised in order to obtain the highest Raman signal (Mercier et al., 2009). At least three spectra were acquired for each sample. 160 The  $CO<sub>2</sub>$  content in the glass was quantify using the calibration method of Morizet et al. 161 (2013), which provided a reproducibility on the  $CO<sub>2</sub>$  measurements of ~5% relative, 162 corresponding to an estimated absolute error on the  $CO<sub>2</sub>$  measurements less than 1 wt% for the investigated samples.

## **3.3 Elemental Analyser**

 We used a Thermo Scientific, Flash 2000, CHNS elemental analyser to measure water (as H) 167 and  $CO<sub>2</sub>$  (as C) in all experimental products. About 1 mg of sample was loaded together with 1 mg of vanadium pentoxide in a tin capsule folded and analysed by combustion at 1800°C. The analyser was calibrated directly prior to analysis and reproducibility on external

170 standards (marble, dolomite and hydrated basalt) was found to be better than 2% for C and 171 10% for H, giving an estimated error on the  $CO_2$  measurement of  $< 1$  wt%.

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#### 173 **3.4 Gravimetric Weight loss**

 After experiments the capsules were weighed using a high precision balance before and after 175 puncture, to measure the mass of  $CO<sub>2</sub> (\pm H<sub>2</sub>O)$  in the excess fluid phase from which, the mass 176 of dissolved  $CO<sub>2</sub>$  in the glass can be calculated by mass-balance. The error associated with this technique depends largely on the initial amount of material loaded in the capsule. Considering a maximum error on the weight measurements of 0.5 mg, for a minimum amount 179 of loaded material of 30 mg, the error on the subsequent  $CO_2$  estimate by this method is  $< 2$  wt%. There may also be an under-estimation of fluid phase mass if some is retained in enclosed bubbles. However, most vesicles are found at the capsule wall (see Fig 1); as a result, most of the fluid must be released on piercing.

# 183 **4. RESULTS**

184 All experimental charges were  $CO<sub>2</sub>$  saturated. This was attested by the presence of bubbles in 185 all investigated charges (Fig.1) and by weight loss after piercing the capsules. All results 186 from solubility experiments are reported in Table 2 with  $CO<sub>2</sub>$  content estimated from 187 elemental analyser, weight loss (after capsule puncture), EMPA and micro-Raman 188 spectroscopy. A comparison of the four different methods used to measure the  $CO<sub>2</sub>$  content of 189 the experimental charges is presented in Fig. S2. This figure shows that the agreement 190 between the Raman, elemental analyser and gravimetric weight loss methods is very good. 191 Estimates from EMPA shortfall are consistently overestimating the amount of  $CO<sub>2</sub>$  even after 192 correction for H2O (determined by elemental analyser), suggesting that using EMPA shortfall 193 to estimate the melt  $CO<sub>2</sub>$  content might be inaccurate. Unless stated otherwise, all  $CO<sub>2</sub>$ 

194 contents reported in the following figures are from measurements using the elemental 195 analyser. The results of  $CO<sub>2</sub>$  solubility experiments at 350 MPa for a range of compositions 196 are reported in Fig. 2 together with a data point from an earlier study using a similar 197 composition (Iacono-Marziano et al., 2012). Fig.2 clearly shows a decrease in  $CO<sub>2</sub>$  solubility 198 with increasing amount of network forming cations  $(Si^{4+}$  and  $Al^{3+})$ . This decrease appears to 199 be smooth and continuous across the transitional field. The effect of pressure, that is 200 nominally the pressure of  $CO<sub>2</sub>$ , on solubility is shown in Fig. 3 for starting compositions at 18 201 to 41 wt%  $SiO<sub>2</sub>$  (SiO<sub>2</sub> + Al<sub>2</sub>O<sub>3</sub> of 21 to 51 wt% respectively, expressed with volatiles at 202 saturation at 350 MPa). Since experiments at 50 MPa could not be quenched fast enough to 203 prevent the growth of quench crystals,  $CO<sub>2</sub>$  solubility was estimated from the amount of gas 204 released after capsule puncture and their  $CO<sub>2</sub>$  contents are therefore associated with a larger 205 error (estimated at  $\pm 2$  wt%) than those determined by elemental analyser (estimated at  $\lt 1$ 206 wt%). At 18 wt%  $SiO<sub>2</sub>$  (at the edge of the carbonate field) a pressure drop from 1500 to 180 207 MPa seems to have a limited effect on the solubility of  $CO_2$  (25 to 20 wt%  $CO_2$ ) and most of 208 the solubility drop takes place from 100 to 0.1 MPa (assuming no  $CO<sub>2</sub>$  remains in the melt at 209 0.1 MPa). This results in a strongly non-linear dependence of  $CO<sub>2</sub>$  solubility with pressure for 210 melt compositions with  $SiO_2$  contents in the range 18-30 wt%. At  $SiO_2$  content higher than 30 211 wt% the solubility dependence on pressure (from 350 to 0.1 MPa) is linear, as expected in 212 silicate melts for the pressure range considered.

#### 213 **5. DISCUSSION**

 Evidence for a genetic connection between kimberlite and carbonatite magmas goes beyond their, long noticed, spatial and temporal occurrence (e.g. Janse, 1975; Mitchell, 2005; White et al., 1995). Kimberlite and carbonatite melts can both be produced by very low degree partial melting of a carbonated mantle source as inferred from their high concentration of

 incompatible trace elements (Nelson et al., 1988) and from high pressure melting experiments of carbonated peridotite phase assemblages (Dalton and Presnall, 1998; Dasgupta and Hirschmann, 2006; Ghosh et al., 2009; Gudfinnsson and Presnall, 2005; Rohrbach and Schmidt, 2011). In addition kimberlite and carbonatite melts have been argued to be related by fractionation processes (Dalton and Presnall, 1998; Dawson and Hawthorne, 1973; Larsen and Rex, 1992). This clear link between the two types of magma supports the hypothesis of Brooker et al. (2011) that kimberlite primary magmas were originally more transitional or carbonatitic in composition. The set of transitional synthetic super-liquidus melt compositions that have been produced here should therefore yield a robust approximation of 227 the solubility law for  $CO<sub>2</sub>$  in primary kimberlitic melts.

## **5.1 Empirical model of CO<sup>2</sup> solubility in carbonated melts**

 Based on the solubility experiments presented here and literature data we developed a purely 231 empirical model of  $CO<sub>2</sub>$  solubility as a function of the amount of network forming cations (SiO<sub>2</sub> + Al<sub>2</sub>O<sub>3</sub>) and pressure. We emphasised that it is the first modelling effort addressing such low silica melt compositions. The simple model is defined as a third order polynomial 234 linking the amount of CO<sub>2</sub> dissolved in the melt to the  $SiO_2 + Al_2O_3$  content and in which each coefficient is in turn a function of pressure as follow:

236 
$$
CO_{2wt\%} = A \times (\text{SiO}_2 + \text{Al}_2\text{O}_3)^3 + B \times (\text{SiO}_2 + \text{Al}_2\text{O}_3)^2 + C \times (\text{SiO}_2 + \text{Al}_2\text{O}_3) + D
$$
 (1)  
237 Where:

 $A = a \times P^b$ 

 $B = c \times P^d$ 

$$
C = e \times P^f
$$

 With *D*, *a*, *b*, *c*, *d*, *e* and *f* representing adjusted parameters reported in Table 3. The rationale behind the formulation of equation (1) is to simulate a pressure-dependent process of dilution  from a pure carbonate end-member (*D*=50) with the addition of network-forming cations 241 (SiO<sub>2</sub> and Al<sub>2</sub>O<sub>3</sub>). In order to adjust the parameters in equation (1), we used CO<sub>2</sub> solubility data for basalt (Mattey, 1991; Pawley et al., 1992; Shishkina et al., 2010; Stolper and Holloway, 1988), haplo-phonolite (Morizet et al., 2002), phonotephrite (Behrens et al., 2009), melilitite (Brooker et al., 2001) in addition to selected data from Brey and Ryabchikov, (1994); Brooker, (1995); Brooker et al., (2011); Brooker and Kjarsgaard, (2011); Iacono- Marziano et al., (2012); Morizet et al., (2013); Morizet et al., (2014) and this study (all shown in the subsequent figures). Equation (1) reproduces our experimental data well (standard 248 deviation of 0.9 wt%  $CO<sub>2</sub>$  between the modelled and measured values) and allow us to 249 explore a larger P- $X_{(SiO2 + A12O3)}$  space. Fig. 4 shows the modelled solubility of CO<sub>2</sub> as a 250 function of pressure for compositions ranging from  $SiO_2 + Al_2O_3$  of 0 to 51 wt% and pressure 251 from 1500 to 10 MPa. Fig.4 shows the gradual change in the  $CO_2$  solubility behaviour from carbonate to silicate end-member melts as a function of pressure. We note that from Fig.4, a typical transitional melt enters the kimberlite "root zone" (see the classical model from 254 Hawthorne, 1975) with a  $CO<sub>2</sub>$  content of 10 to 18 wt%, consistent with the "target value" of 15 wt% determined by Brooker et al. (2011) for kimberlites.

 The range of experiments presented here is not extensive enough to incorporate the effect of temperature and alkali content in equation (1). For this, we considered the available from the 259 literature. Fig. 5 compares data from a range of studies and shows the evolution of  $CO<sub>2</sub>$ 260 solubility as a function of network forming cations  $(SiO<sub>2</sub>+Al<sub>2</sub>O<sub>3</sub>)$  for a large range of composition and pressure from 2000 to 50 MPa. The predicted evolution from equation (1) is also shown for pressure between 2000 and 20 MPa. The melt composition of all data shown in Fig 5 is reported in Table S2, where one can notice the wide range of compositions 264 explored by these various studies. The variety of methods used to estimate the  $CO<sub>2</sub>$  content in  these studies (EMP shortfall, Raman, FTIR, elemental analyser and gas chromatography), makes the comparison of dataset not ideal. In addition, while the present study, that of Iacono-Marziano et al., (2012), Morizet et al., (2014), Brooker et al., (2001) and Brey and Ryabchikov, (1994) are from super-liquidus experiments, data from Brooker *et al.,* (2011) are from patches of glass in mostly crystallised charges while data from Brooker and Kjarsgaard (2011) and Brooker (1995) are from silicate melts coexisting with an immiscible carbonate 271 melt. Perhaps most importantly, the  $CO<sub>2</sub>/H<sub>2</sub>O$  ratio varies widely over the reported dataset with volatile component in experiments from Iacono-Marziano et al., (2012) and Morizet et 273 al., (2014) being dominated by  $H_2O$ . Keeping in mind these limitations in the comparison, we can see that the set of data from Morizet et al. (2014) at 350 and 100 MPa and Morizet et al. (2013) at 1000 MPa are well reproduced by our model. A similar agreement is noted with the data at 2000 MPa from Brooker et al., (2001), at 200 MPa from Brooker et al (2011) and (to a lesser extent) at 1500 MPa from Brooker (1995). We also note that data at 1000 MPa from Brey and Ryabchikov (1994) (we only report experimental data at 1000 MPa where they reported clear glass) are also well reproduced despite the significant difference in terms of chemical composition (MgO up to 27wt%). Fig 6, shows a plot of experimentally determined 281 vs. calculated  $CO_2$  solubility from which it appears that the highest deviation from the model are for data by Brooker et al (2011) and Brooker and Kjarsgaard (2010). We made several 283 attempt to link the deviation from the modelled value to the melt composition  $(Na<sub>2</sub>O, K<sub>2</sub>O,$  Na<sub>2</sub>O+K<sub>2</sub>O, SiO<sub>2</sub>/Al<sub>2</sub>O<sub>3</sub>) but could not find any robust correlations. There is however a hint 285 that melt compositions rich in alkali can incorporate more  $CO<sub>2</sub>$  than comparatively Ca and Mg-rich compositions (see in Fig. 5 the isolated experiment from Brooker (1995) at 1500 287 MPa with 15.6 wt%  $CO_2$  and a composition of 0 wt% CaO and 37 wt% Na<sub>2</sub>O). As additional experimental data become available, future models should be able to explore the full effect of 289 composition (in term of Mg, Ca, Na, K, Fe cations) on  $CO<sub>2</sub>$  solubility.

290 A strong correlation was found between the method used to determine  $CO<sub>2</sub>$  content and 291 deviation from our model value. Indeed, 70% of the data located further than two standard 292 deviations away from their calculated value had  $CO<sub>2</sub>$  content determined by shortfall of 293 EMPA analyses. Comparing our own EMPA shortfall measurements to  $CO<sub>2</sub>$  determined by 294 bulk analyser (Fig. S2), we observe that determining the  $CO<sub>2</sub>$  content by EMPA shortfall can 295 lead to an overestimation of 2 to 6 wt%  $CO<sub>2</sub>$ . We therefore conclude (i) that most of the 296 literature data yielding  $CO<sub>2</sub>$  solubility values that deviates from our model can be attributed to 297 the large error associated with estimating  $CO<sub>2</sub>$  content from EMPA shortfall and (ii) that from 298 the current, limited, dataset there is no identifiable systematic deviations related to the melt 299 composition. Equation (1) therefore provides a good first order approximation of the  $CO<sub>2</sub>$ 300 content of carbonated melt over a large range of composition ( $SiO_2 < 55$  wt%; Na<sub>2</sub>O+K<sub>2</sub>O < 301 22 wt%). The entrapment pressure of recently reported  $CO<sub>2</sub>$ -rich melt inclusions from 302 Oldoinyo Lengai (de Moor et al., 2013) for instance, can be estimated using equation (1) 303 (yielding an entrapment depth of 265 to 2085 MPa for inclusions containing 3 to 8 wt%  $304$  CO<sub>2</sub>).

305

# 306 **5.2 Implications for Kimberlite ascent and volcanism**

307 As hypothesised by Brooker et al  $(2011)$  our results indicate that  $CO<sub>2</sub>$  solubility decreases with increasing amount of network forming cations over the carbonate-silicate transitional field. This finding supports the conclusions of Russell et al., (2012) that an ascending carbonate melt, assimilating mantle orthopyroxene (OPX) and becoming progressively 311 enriched in silica, will release an increasing amount of  $CO<sub>2</sub>$  into the gas phase and promote magma ascent by keeping it buoyant in spite of increasing xenocryst loading. The effect of pressure (shown in Fig. 3 and 4) on transitional melts appears to be a function of their composition; melts with a composition closer to the carbonate end-member retain a large 315 quantity of  $CO_2$  until very shallow (3 km) depth while slightly more silicate-rich melts show a continuous and progressive degassing profile with  $CO<sub>2</sub>$  being equally released from mantle depth to the surface. The solubility-pressure relationships shown by the transitional melt compositions in Fig. 3 and 4 are intermediate between the behaviour of a carbonate melt which will show little pressure dependence on solubility, and that of a typical silicate melt which will show a mostly linear relationship in the pressure range considered (Fig. 3, 4,e.g. Papale et al., 2006; Iacono-Marziano et al 2012).

323 The behaviour of transitional melts, retaining more than 18 wt%  $CO<sub>2</sub>$  up until very shallow depth should lead to a rapid increase in ascent velocity while reaching the last 3 km depth where important quantities of  $CO<sub>2</sub>$  will be released (Fig. 4). This acceleration will be exacerbated by the fact that the volume fraction of gas will reach values higher than 77%, corresponding to the point at which the bubble foam will collapse (Woods, 1995) changing the continuous phase from a bubbly liquid magma to an ash-laden gas and therefore considerably increasing the flow speed as the frictional force become much smaller and the viscosity becomes closer to that of the gas phase. This ascent scenario can readily explain some of the typical morphological features of kimberlite pipes. (i) The widening upward geometry of the pipe, typical of eruptions happening at depth, can be explained by the high amount of  $CO<sub>2</sub>$  released over a, most probably, very small time increment leading to overpressure and explosion below the surface. (ii) The appearance of breccias and irregularly 335 shaped blocks at depth of  $\sim$ 3 km, in the "root zone" (see the classical model from Hawthorne, 336 1975) is consistent with large amount of  $CO<sub>2</sub>$  starting to be released at this depth and the associated rapid volumetric expansion (Fig. 4). The occurrence of hypabyssal intrusions of kimberlites however suggests that some kimberlite stall during their ascent through the crust. Although we cannot confidently assign a reason for this, possibilities include the loss of  volatiles, segregating from the magma during ascent or the progressive cooling of the magma (Kavanagh and Sparks, 2009), both process inducing crystallisation and greatly increasing magma viscosity. Experiments on these compositions suggest that crystallisation is extremely rapid, as illustrated by the speed at which quench crystals formed in some of our experiments. 

 While  $CO<sub>2</sub>$  is the most abundant volatile in kimberlite magmas, an unknown but probably significant amount of water is also dissolved in these melts (up to 10 wt%; Kopylova et al., 2007; also see discussion in Sparks et al., 2009 and experimental investigation by Keppler, 2003). Water degassing is therefore likely to exert a large influence on the ascent dynamics of Kimberlite melts. It remains unclear however whether this process would enhance, limit or displace the depth at which the CO<sub>2</sub>-exsolution-triggered acceleration of kimberlite melts that we predict takes place.

# **6. CONCLUSIONS**

354 We have determined  $CO_2$  solubility laws for kimberlite melt and have also provided a general 355 solubility model for carbonated melt composition ( $SiO<sub>2</sub> < 55$  wt%) at pressure between 50 356 and 1500 MPa. We found that (i)  $CO<sub>2</sub>$  solubility decreases steadily with increasing amount of 357 network forming cations (ii) The effect of pressure on  $CO<sub>2</sub>$  solubility is a strong function of 358 composition with low  $SiO<sub>2</sub>$  melts retaining large amount (~15 wt%) of  $CO<sub>2</sub>$  up to very 359 shallow pressure (~100 MPa) while more silicated melts have a near linear  $CO_2$  solubility dependence on pressure. We propose that this peculiar pressure-solubility dependency should result in a strong acceleration of an ascending kimberlite magma in the last 3 km of crust where  $CO<sub>2</sub>$  starts to exsolve in large quantities. This behaviour can explain morphological features of kimberlite pipes, notably the depth extent of the root zone and the widening upward shape of the conduit and can account for the highly explosive character of Kimberlite eruptions.

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## **TABLES**

**Table 1**: Starting oxide and natural rock powder mix compositions. The composition of a

natural lamproite from Torre Alfina, Italy, (Peccerillo et al., 1998), fused twice at 1400°C and

used to prepare the oxide-mix compositions is reported at the top of the table.

```
507 Table 2: Run conditions, EMPA analyses (averaged from 20), H2O determined by elemental
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508 analyser (Flash) and  $CO_2$  determined from: (i) EMPA (by subtracting H<sub>2</sub>O content to EMPA

shortfall), (ii) Elemental analyser (Flash), (iii) Micro-Raman spectroscopy (following the

method of Morizet et al., (2013) and (iv) Weight loss measured by puncturing the capsule

511 (allowing the  $CO<sub>2</sub>$  to escape) after each run. Run duration was of 2 hours in all experiments.

 **Table 3**: Adjusted parameters (and corresponding standard error on multiple non-linear 514 regression fit) to calculate  $CO<sub>2</sub>$  solubility from Eq. (1)

## **FIGURES**

 **Figure 1:** Optical microphotograph showing the results from various supra-liquidus experimental run producing a pure glass in all cases excepted for sample TA6\_1\_5 (lower right) in which quench crystals give a "milky" aspect to the otherwise glassy product. All samples shown are synthesised in IHPV apparatus excepted sample TA6\_1\_5 which was synthesised with piston cylinder. Corresponding SEM images are shown in Fig S1.

523 **Figure 2**: CO<sub>2</sub> solubility measurements for a series of compositions across the silicate to 524 carbonate melt transitions equilibrated at 350 MPa. The  $SiO<sub>2</sub>+Al<sub>2</sub>O<sub>3</sub>$  content is reported  $525$  including volatiles. For most experiments,  $CO<sub>2</sub>$  content is estimated from elemental analyser 526 and associated error is estimated at  $\pm$  1 wt%. CO<sub>2</sub> content from Iacono-Marziano et al., 527 (2012) is estimated from FTIR analyses.

528

**Figure 3**:CO<sub>2</sub> solubility as a function of pressure for three Kimberlite/Transitional and two 530 silicate melt compositions spanning  $SiO<sub>2</sub>$  content of 18 to 41 wt% and  $SiO<sub>2</sub> + Al<sub>2</sub>O<sub>3</sub>$  content 531 of 21 to 51 wt% respectively (calculated including volatiles and corresponding to  $SiO<sub>2</sub>$  + Al<sub>2</sub>O<sub>3</sub> contents of 27 to 54 wt% on a volatile-free basis). The light-brown to green colour part of the plot represents the upper 3 km of crust, corresponding to the typical "root zone" of Kimberlites. Dashed lines are fitted by eye through the data points.

535

536 **Figure 4**: Modelled evolution of CO<sub>2</sub> solubility as a function of pressure using equation (1) 537 for melt compositions ranging from 0 to 41 wt%  $SiO_2$  and 0 to 51 wt%  $SiO_2 + Al_2O_3$ . 538 Experiments of corresponding chemistry are shown as squares of matching colour.

539

**Figure 5**: CO<sub>2</sub> solubility measurements from this study and the literature for compositions across the silicate to carbonate melt transition, equilibrated at 2000, 1500, 350, 200, 100 and 50 MPa. Literature data are from Brooker and Kjarsgaard, 2011; Brooker et al., 2011; Iacono- Marziano et al., 2012; Brooker et al., 2001; Brooker 1995; Morizet et al., 2013 Morizet et al., 2014 and Brey and Ryabchikov, 1994. Note that literature data are reported using the 545 experiment total pressure and not the  $P_{CO2}$ . Model prediction values from equation (1) are shown for a range of pressure (2000 to 20 MPa) as dotted black curves.

548 **Figure 6**: Experimentally determined vs. calculated CO<sub>2</sub> solubility using equation (1). Doted 549 red line represent the 1:1 line while continuous red lines on either sides represent the  $\pm 2\sigma$ deviation.

# **SUPPLEMENTARY INFORMATION**

**TableS1:** Standard deviation for EMP analyses reported in Table 2 (n=20).

555 **Table S2**: Run conditions, EMPA analyses and  $CO_2$  determined from Raman or by bulk  $CO_2$ 

LECO analyser for experiments from Brooker et al., (2011); Brooker and Kjarsgaard, (2011);

Iacono-Marziano et al., (2012); Brooker (1995) and Morizet et al., (2014).

 **Figure S1:** Scanning electron microscopy (SEM) images of experimental charges shown in Fig. 1. All run produced a pure glass, excepted sample TA6\_1\_5 (lower right) in which quench crystals are pervasive.

563 **Figure S2:**Comparison between  $CO<sub>2</sub>$  content in experimental charges determined by (i) 564 EMPA (by subtracting  $H_2O$  content to EMPA shortfall), (ii) Elemental analyser (Flash), (iii) Micro-Raman spectroscopy (following the method of Morizet et al., 2013), (iv) Weight loss 566 measured by puncturing the capsule (allowing the  $CO<sub>2</sub>$  to escape) after each run and (v) EMPA shortfall without correction.



**Table 1**: Starting oxide and natural rock powder mix compositions. The composition of a natural lamproite from Torre Alfina, Italy, (Peccerillo et al., 1998), fused twice at 1400°C and used to prepare the oxide-mix compositions is reported at the top of the table.



Table 2: Run conditions, EMP analyses (averaged from 20), H<sub>2</sub>O determined by elemental analyser (Flash) and CO<sub>2</sub> determined from: (i) EMPA (by subtracting H<sub>2</sub>O content to EMPA shortfall), (ii) Elemental analyser (Flash), (iii) Micro-Raman spectroscopy (following the method of Morizet *et al.*, 2013) and (iv) Weight loss measured by puncturing the capsule (allowing the  $CO<sub>2</sub>$  to escape) after each run . Run duration was of 2 hours in all experiments.



**Table 3**: Adjusted parameters (and corresponding standard error on multiple non-linear regression fit) to calculate CO<sub>2</sub> solubility from Eq. (1). Regression was calculated from over 160 data points (detail in text).

![](_page_25_Picture_0.jpeg)

# Figure 1. Moussallam et al.

![](_page_26_Figure_0.jpeg)

**Figure 2, Moussallam et al.**

![](_page_27_Figure_0.jpeg)

**\***(by elemental analyser and weight loss)

**Figure 3, Moussallam et al.**

![](_page_28_Figure_0.jpeg)

**Figure 4, Moussallam et al.**

![](_page_29_Figure_0.jpeg)

**Figure 5, Moussallam et al.**

![](_page_30_Figure_0.jpeg)

(calulated from equation 1)

# **Figure 6, Moussallam et al.**

![](_page_31_Picture_0.jpeg)

Figure S1. Moussallam et al.

![](_page_32_Figure_0.jpeg)

**Figure S2, Moussallam et al.**