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# A revised pseudo-second order kinetic model for adsorption, sensitive to changes in adsorbate and adsorbent concentrations

<sup>1\*</sup>Jay C. Bullen; <sup>1</sup>Sarawud Saleesongsom; <sup>2</sup>Kerry Gallagher; and <sup>1,3\*</sup>Dominik J. Weiss

<sup>1</sup>Department of Earth Science and Engineering, Imperial College London, London SW7 2AZ, United Kingdom

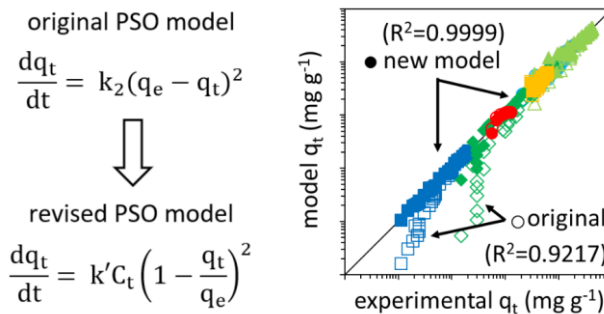
<sup>2</sup>Géosciences/OSUR, University of Rennes, Rennes, 35042, France

<sup>3</sup>Civil and Environmental Engineering, Princeton University, United States of America

\*Corresponding authors:

Email: [j.bullen16@imperial.ac.uk](mailto:j.bullen16@imperial.ac.uk); [d.weiss@imperial.ac.uk](mailto:d.weiss@imperial.ac.uk)

## Graphical Abstract



## Keywords

Adsorption kinetics; kinetic model; pseudo-second order; Lagergren; water treatment; particle size

22

## Abstract

23 The development of new adsorbent materials for the removal of toxic contaminants from drinking  
24 water is crucial to achieving the United Nations Sustainable Development Goal 6 (clean water and  
25 sanitation). The characterisation of these materials includes fitting models of adsorption kinetics to  
26 experimental data, most commonly the pseudo-second order (PSO) model. The PSO model,  
27 however, provides no sensitivity to changes in experimental conditions such as adsorbate and  
28 adsorbent concentrations ( $C_0$  and  $C_s$ ) and consequently is not able to predict changes in performance  
29 as a function of operating conditions. Furthermore, the experimental conditionality of the PSO rate  
30 constant,  $k_2$ , can lead to erroneous conclusions when comparing literature results. In this study, we  
31 analyse 108 kinetic experiments from 47 literature sources to develop a relatively simple  
32 modification of the PSO rate equation, yielding:

$$\frac{dq_t}{dt} = k' C_t \left(1 - \frac{q_t}{q_e}\right)^2$$

33 Unlike the original PSO model, this revised rate equation (rPSO) demonstrates the first-order and  
34 zero-order dependencies upon  $C_0$  and  $C_s$  that we observe empirically. Our new model reduces the  
35 residual sum of squares by 66% when using a single rate constant to model multiple adsorption  
36 experiments with varying initial conditions. Furthermore, we highlight how the rPSO rate constant  $k'$   
37 is more appropriate for literature comparison, highlighting faster kinetics in the adsorption of  
38 arsenic onto alumina versus iron oxides. This revised rate equation should find applications in  
39 engineering studies, especially since unlike the PSO rate constant  $k_2$ , the rPSO rate constant  $k'$  does  
40 not show a counter-intuitive inverse relationship with the increasing reaction rate when  $C_0$  is  
41 increased.

## 42 Introduction

43

44 There is a wealth of recent literature concerning the development of novel adsorbent materials for  
45 the remediation of contaminated water, such as composite materials offering superior stability <sup>1</sup>,  
46 ease of separation from the effluent <sup>2 3</sup>, or multifunctional capabilities such as photocatalytic activity  
47 <sup>4 5</sup>. Energy input typically forms about one third of water treatment plant operation costs <sup>6</sup>, and if  
48 energy efficiencies are to be improved then accurate models of adsorption kinetics (including rate  
49 constants) are needed to (a) identify the minimum duration needed for batch treatments and (b)  
50 estimate maximum flow rates for column or continuous-flow treatments <sup>7</sup>. Laboratory experiments  
51 can only partially capture the environments in which new adsorbents will operate, and in practice  
52 different concentrations of adsorbent ( $C_s$ ) will be needed to treat different concentrations of  
53 contaminant in the influent ( $C_0$ ). It is thus important that adsorption models are made sensitive to  
54 operating conditions, providing predictive capabilities.

55 The pseudo-second order (PSO) rate equation <sup>8</sup>, popularised by Ho and McKay (1999) <sup>9</sup>, is probably  
56 the most popular model currently used to describe adsorption kinetics <sup>10</sup>. The PSO rate equation  
57 takes the form:

$$\frac{dq_t}{dt} = k_2(q_e - q_t)^2$$

58

*Equation 1*

59 where  $t$  is time (minutes),  $q_t$  is the amount of adsorbate adsorbed per mass of adsorbent at time  $t$   
60 ( $\text{mg g}^{-1}$ ),  $k_2$  is the pseudo-second order rate constant ( $\text{g mg}^{-1} \text{min}^{-1}$ ), and  $q_e$  is the amount of  
61 adsorbate adsorbed at equilibrium ( $\text{mg g}^{-1}$ ) <sup>9</sup>.

62 The decrease in the concentration of aqueous adsorbate with time is given by the equation:

$$C_t = C_0 - C_s q_t$$

63

*Equation 2*

64 where  $C_t$  is the concentration of aqueous adsorbate at time  $t$  ( $\text{mg L}^{-1}$ ),  $C_0$  is the initial adsorbate  
65 concentration at  $t=0$  ( $\text{mg L}^{-1}$ ) and  $C_s$  is the concentration of adsorbent ( $\text{g L}^{-1}$ ).

66 The PSO model is popular for several reasons. Firstly, it has a simple mathematical form. Secondly,  
67 despite being applied by Ho and McKay as a mechanistic model for the bidentate adsorption of  
68 copper onto peat <sup>11</sup>, the PSO model is able to fit kinetic data for a wide range of systems with  
69 different reaction mechanisms <sup>9 12 13</sup> (including where diffusion control is to be expected <sup>14</sup>). Thirdly,  
70 Equation 1 can be integrated and rearranged to provide linear equations (of the form  $y=mx+c$ ) from  
71 which the model parameters  $k_2$  and  $q_e$  can be easily obtained by linear regression <sup>15</sup>.

72 However, the PSO model has several important limitations due to the absence of adsorbate and  
73 adsorbent parameters within the rate equation, with  $k_2$  and  $q_e$  parameters being valid only under  
74 the specific experimental conditions under which the PSO model was fitted. The first limitation is  
75 that the model cannot predict how adsorption kinetics will change as a function of  $C_0$  and  $C_s$ , limiting  
76 its application in engineering or optimisation studies. Furthermore, rate constants from different

77 literature sources with different experimental conditions cannot be meaningfully compared: greater  
78 values of  $k_2$  do not necessarily indicate adsorbents possessing superior adsorption kinetics.

79 The aim of the present study was to modify the popular PSO equation, introducing sensitivity  
80 towards changes in  $C_0$  and  $C_s$ , with the objective of both improving predictive capabilities for  
81 engineering studies, and normalising rate constants for easier comparison between literature  
82 sources. The PSO model does not necessarily reveal insights into the adsorption mechanisms (i.e.  
83 whether intraparticle diffusion or chemisorption is the rate determining step)<sup>13 16</sup>, and our aim was  
84 similarly to develop an empirical model, rather than a mechanistic model. We thus conducted an  
85 empirical analysis of the adsorption kinetics reported by the literature to assess the influence of  $C_0$   
86 and  $C_s$  on adsorption rates, and to modify the PSO rate equation accordingly.

87 We used the method of initial rates to determine the order of reaction with respect to both  $C_0$  and  $C_s$   
88 (given the possibility for data at later times to disguise the true reaction order<sup>17</sup>, such as when  
89 slower surface precipitation processes coincide with monolayer adsorption<sup>18</sup>). We first performed  
90 quality control experiments, investigating various methods for calculating initial rates when the  
91 availability of early kinetic data is limited (as per many adsorption experiments). We then compiled a  
92 wide range of literature data sets wherein multiple adsorption kinetic experiments with different  
93 values of  $C_0$  and  $C_s$  are reported (with each data set being a specific adsorbate-adsorbent system)  
94 and determined the order of reaction with respect to each variable. We used mineral and organic  
95 adsorbents, and metal, inorganic and organic adsorbates, to achieve a model that is generally  
96 applicable to a wide range of systems, as per the original PSO model. We built the observed  $C_0$  and  
97  $C_s$  dependence into a revised form of the PSO rate equation (which we refer to as *rPSO*) and verified  
98 that the rate constants given by this new model are more stable with respect to changes in  
99 experimental conditions than the PSO rate constant  $k_2$ . Finally, we used two application studies to  
100 assess the potential of this revised PSO model to overcome current limitations: (1) describing  
101 multiple experiments with varying values of  $C_0$  and  $C_s$  using a single rate constant, and (2) achieving a  
102 more meaningful comparison of the adsorption kinetics reported across the literature.

## 103 Experimental

104

### 105 Data sets

106 Literature sources that experimentally investigated the influence of  $C_0$ ,  $C_s$  or particle size upon  
 107 adsorption kinetics were compiled and the experimental data tabulated (referenced in the  
 108 Supplementary Information: SI Table S1). Both mineral adsorbents and organic adsorbents (activated  
 109 carbon and chitosan) were included, however zeolites and metal-organic frameworks (MOFs) were  
 110 not since the sorption mechanism of adsorbate trapping within cages might produce contrary  
 111 results. None of the literature sources found gave any mechanistic account or mathematical  
 112 explanation for observed differences in adsorption kinetics due to varying values of  $C_0$ ,  $C_s$  or particle  
 113 size. The majority of the compiled literature used the PSO model to describe adsorption kinetics.

114 In total 47 literature sources with approximately 100 kinetic experiments were collected. This  
 115 includes: 14 literature sources with early kinetic data (where  $0 < \frac{q_t}{q_e} < 0.2$ ) to investigate the  
 116 influence of early data availability on calculations of the initial rate; 8 literature sources (9 data sets)  
 117 with a total 37 experiments where  $C_0$  is varied; 6 literature sources (8 data sets) with a total 27  
 118 experiments where  $C_s$  is varied; and 21 literature sources (25 experiments) for the adsorption of  
 119 inorganic arsenic onto iron oxide and alumina adsorbents. A data set is considered to be all kinetic  
 120 experiments using the same adsorbate-adsorbent system within a single literature source. The  
 121 compiled data sets are available elsewhere <sup>19</sup>.

122

### 123 Mathematical approaches for the determination of initial rates

124 Three approaches towards the calculation of initial rates were compared: (1) the initial slope, (2)  
 125 linearised PSO kinetics, and (3) non-linear PSO kinetics.

126 In the initial slope approach, the initial rate ( $\frac{\Delta q_t}{\Delta t}$  at  $t=0$ ) was calculated as the slope between the  
 127 origin at (0,0) and the earliest available data point at  $t>0$  <sup>20</sup>.

128 Initial rates were also calculated using the following linearised form of the integrated PSO rate  
 129 equation:

$$\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \frac{t}{q_e}$$

130

*Equation 3*

131 Kinetic profiles were plotted as  $\frac{t}{q_t}$  as a function of  $t$  and the linear regression was obtained using the  
 132 LINEST function in Excel (where the residual sum of squares between the data points and the linear  
 133 regression is minimised). The equilibrium adsorption parameter  $q_e$  was obtained via the relationship  
 134  $q_e = \frac{1}{m}$  where  $m$  is the slope of the linear regression, and  $k_2$  via  $k_2 = \frac{1}{c \cdot q_e^2}$  where  $c$  is the y-intercept.  
 135 The initial rate of adsorption was then calculated through the simplification of Equation 1:

$$136 \text{ Initial rate} = \frac{dq_{t=0}}{dt} = k_2 q_e^2$$

137

*Equation 4*

138 Uncertainties in  $k_2$ ,  $q_e$  and the initial rate were calculated by linear propagation of the standard  
139 errors in  $m$  and  $c$  given by the LINEST function.

140 Finally, initial rates were calculated using non-linear PSO kinetics. Non-linear fitting of the PSO model  
141 to experimental data was achieved by using Microsoft Excel's Solver function to optimise  $k_2$  and  $q_e$   
142 values, minimising the sum of squared residuals between the model and experiment. Uncertainties  
143 in  $k_2$  and  $q_e$  were calculated using a Monte-Carlo approach with 200 simulations as described by Hu  
144 *et al.*<sup>21</sup>.

145 For all literature sources, parameters were recalculated to the same units for ease of comparison:  $k_2$   
146 ( $\text{g mg}^{-1} \text{min}^{-1}$ );  $q_e$  ( $\text{mg g}^{-1}$ ); and the initial rate ( $\text{mg g}^{-1} \text{min}^{-1}$ ).

147 The influence of the availability of early kinetic data on the accuracy and precision of initial rates  
148 calculated using these three approaches was evaluated as follows. Fourteen data sets containing  
149 early kinetic data were collected (defined as adsorption experiments containing data within the  
150 range  $0 < \frac{q_t}{q_e} < 0.2$ ). Initial rates were then re-calculated as data points were consecutively removed  
151 from the earliest to the latest. A linear regression between the calculated initial rates and the value  
152 of  $\frac{q_t}{q_e}$  at the first available kinetic data was determined and extrapolated to  $\frac{q_t}{q_e} = 0$  to provide a  
153 theoretical 'true' initial rate (representing if kinetic data were to be collected within an  
154 infinitesimally small time period). This theoretical 'true' initial rate was used as a reference value to  
155 determine variation in the calculated initial rate as a function of the availability of early kinetic data.  
156 A systematic error was calculated using the average error across all data sets and a random error  
157 was calculated as the standard deviation in the error across all data sets. The significance of the  
158 differences observed in the initial rate errors given by the three mathematical approaches was  
159 determined using the paired samples t-test.

160 After evaluating the three approaches (see Results and Discussion), non-linear PSO kinetics were  
161 used to determine initial rates in all subsequent calculations.

162

### 163 **Determining the order of reaction**

164 The order of reaction with respect to the independent variables  $C_0$  and  $C_s$  was calculated as the slope  
165 of  $\log(\text{initial rate})$  versus  $\log(\text{independent variable})$ <sup>22</sup>. The order of reaction was calculated for each  
166 data set (kinetic experiments using the same adsorbate-adsorbent system within a single literature  
167 source), with each data point used within the linear regression representing a single kinetic  
168 experiment at a unique value of  $C_0$  or  $C_s$ . This is represented by the equation:

$$\text{order of reaction} = \frac{\Delta \log (\text{initial rate})}{\Delta \log (C_0 \text{ or } C_s)}$$

169

*Equation 5*

170 For each data set, the order of reaction with respect to the independent variable was calculated  
171 using the LINEST function in Microsoft Excel. The error for each data set was specified as the  
172 standard error of the slope. An average (mean,  $\bar{x}$ ) order of reaction representing all data sets was

173 calculated, with errors reported as the standard deviation. The dependencies of  $k_2$  and  $k'$  upon  $C_0$   
 174 and  $C_s$  were determined using the same method, only substituting the initial rate with  $k_2$  or  $k'$ .

175

### 176 **Modelling the revised rate equation**

177 Our final rate equation, developed and derived in the Results and Discussion (Equation 11, referred  
 178 to as the rPSO), is:

$$\frac{dq_t}{dt} = k' C_t \left(1 - \frac{q_t}{q_e}\right)^2$$

179

*Equation 6*

180 where the rate constant  $k'$  takes the units  $L g^{-1} min^{-1}$ . As the rPSO rate equation is not easily  
 181 integrated, experiments were simulated using Microsoft Excel. The quantity of adsorbate adsorbed  
 182 at the  $n^{th}$  data point was calculated using the following formula:

$$q_n = q_{n-1} + \left( (t_n - t_{n-1}) \cdot \left( k' C_{t(n-1)} \left(1 - \frac{q_{n-1}}{q_e}\right)^2 \right) \right)$$

183

*Equation 7*

184 The time interval between data points,  $(t_n - t_{n-1})$  or  $\Delta t$ , was reduced until the magnitude of  $\Delta t$  had  
 185 no significant effect on the results. The rPSO parameters  $k'$  and  $q_e$  were obtained by non-linear  
 186 fitting, using Microsoft Excel's Solver function to minimise the residual sum of squared residuals  
 187 between the model and experiment.

188 For all literature sources, parameters were recalculated to the same units for ease of comparison:  $k_2$   
 189 ( $g mg^{-1} min^{-1}$ );  $q_e$  ( $mg g^{-1}$ ); and the initial rate ( $mg g^{-1} min^{-1}$ ).

190

191 KERRR

$$\frac{dq_t}{dt} = k_2 (q_e - q_t)^2$$

192

*Equation 8*

193 where  $t$  is time (minutes),  $q_t$  is the amount of adsorbate adsorbed per mass of adsorbent at time  $t$   
 194 ( $mg g^{-1}$ ),  $k_2$  is the pseudo-second order rate constant ( $g mg^{-1} min^{-1}$ ), and  $q_e$  is the amount of  
 195 adsorbate adsorbed at equilibrium ( $mg g^{-1}$ )<sup>9</sup>.

196 The decrease in the concentration of aqueous adsorbate with time is given by the equation:

$$C_t = C_0 - C_s q_t$$

197

*Equation 9*

198 where  $C_t$  is the concentration of aqueous adsorbate at time  $t$  ( $mg L^{-1}$ ),  $C_0$  is the initial adsorbate  
 199 concentration at  $t=0$  ( $mg L^{-1}$ ) and  $C_s$  is the concentration of adsorbent ( $g L^{-1}$ ).

200 KERRR



201

202

**Application studies**

203 In the first application study (evaluating the potential of the rPSO model for predictive applications),  
204 6 data sets were used: 3 where  $C_0$  was varied and 3 where  $C_s$  was varied. In the first step, values of  
205 the equilibrium adsorption capacity ( $q_e$ ) to constrain the model were obtained by fitting kinetic  
206 experiments individually using the PSO and rPSO models (optimising the rate constant and  $q_e$   
207 simultaneously to minimise the sum of squared residuals). After constraining  $q_e$  to these values, all  
208 experiments within the given data set (i.e. experiments with the same adsorbate-adsorbent system  
209 but different  $C_0$  or  $C_s$  values) were simultaneously fit with the PSO and rPSO models, using a single  
210 rate constant ( $k_2$  or  $k'$ , depending upon the model) to describe all experiments.

211 In the second application study (evaluating the potential of the rPSO rate constant  $k'$  for more  
212 meaningful comparisons across the literature), 18 experiments reporting the adsorption kinetics of  
213 inorganic arsenic onto iron oxide minerals were collated. Both As(V) and As(III) experiments were  
214 included, since no significant difference between the adsorption kinetics was observed. A further 7  
215 experiments reporting the adsorption of inorganic arsenic onto alumina ( $Al_2O_3$ ) were collected for  
216 comparison. The particle radius ( $r$ ) was taken as reported by each study.

## 217 Results and Discussion

218

### 219 Determination of the influence of experimental conditions ( $C_0$ and $C_s$ ) on the 220 initial rate of adsorption

221

#### 222 Quality control: The calculation of initial rates and setting criteria for the selection 223 of literature data sets

224 Many adsorption experiments reported by the literature begin their collection of kinetic data at high  
225 values of  $\frac{q_t}{q_e}$ , where a significant proportion of the reaction has already been completed. This may be  
226 due to challenges in collecting samples quickly (especially when filtering is required) given that many  
227 adsorption reactions reach equilibrium in the minutes timescale. Other possible reasons include a  
228 lack of appreciation over the time-scale at which adsorption kinetics are best measured, with many  
229 papers fitting kinetic models on timescales when the reaction has already plateaued and reached  
230 equilibrium.

231 Whilst we chose to investigate the influence of  $C_0$  and  $C_s$  using the method of initial rates, the lack of  
232 literature reporting early stage kinetic data (i.e. low values of  $\frac{q_t}{q_e}$ ) is a challenge. A popular approach  
233 to calculate initial rates is to determine the slope of a line that is tangent to the experimental data  
234 curve and passes through the origin at (0,0) <sup>20</sup>. However, the later the first kinetic data is collected,  
235 the shallower the slope will be, creating a systematic underestimation of the initial rate. In the most  
236 extreme case, an infinite delay before collection of kinetic data will yield a slope of zero and  
237 subsequently an initial rate of zero. Application of a kinetic adsorption model allows for the  
238 extrapolation of adsorption rates to  $t=0$ , however the accuracy of the calculated initial rates depends  
239 upon how closely the experimental data obeys the applied model.

240 We therefore conducted a preliminary experiment to investigate how a limited availability of early  
241 kinetic data would influence the accuracy and precision of initial rates calculated using the initial  
242 slope or using the original PSO model (given that the PSO model is known to approximately describe  
243 a wide range of adsorbate-adsorbent systems <sup>12</sup>). These results were used to set quality control  
244 criteria for which data sets would be included within the investigation of the influence of  $C_0$  and  $C_s$   
245 on adsorption kinetics.

246 The literature search identified fourteen data sets satisfying the criteria that  $\frac{q_t}{q_e} < 0.2$ , a relatively  
247 small number, highlighting how most authors fail to collect early kinetic data (SI Figure S1). Initial  
248 rates calculated from the slope between the origin and the earliest available data point show the  
249 typical systematic underestimation of initial rates when early kinetic data is missing (Figure 1a, with  
250 the solid line representing the average of all data sets). In contrast, when calculated using the PSO  
251 model, there is no systematic error in the calculation of initial rates when the first kinetic data is  
252 collected in the range  $0 < \frac{q_t}{q_e} < 0.7$  (Figure 1b,c). In all three approaches, significant variation  
253 between data sets is observed, i.e. an error in the initial rate unique to each data set. This error (with  
254 dashed lines representing one standard deviation) is approximately constant in the initial slope  
255 approach, being significant even when early kinetic data is available. In contrast, this error is

256 insignificant using early kinetic data and either of the PSO approaches, however this error increases  
257 in magnitude as early data is sequentially removed.

258 Additionally, the absolute values of the initial rates calculated using the earliest possible kinetic data  
259 were compared (i.e. 14 initial rate calculations), with Student's t-test indicating that both linearised  
260 PSO kinetics and non-linear PSO kinetics tend to return an initial rate greater than that calculated  
261 using the initial slope (with  $p=0.87$  and  $0.97$  respectively). The increase in initial rates calculated  
262 using non-linear PSO kinetics versus linearised PSO kinetics is not significant ( $p=0.33$  using the 14  
263 initial rate calculations). However, when comparing the calculated initial rates with all possible data  
264 cut-offs (i.e. 115 initial rate calculations, Figure 1d) the differences are more significant: non-linear  
265 PSO kinetics return greater initial rates than linearised PSO kinetics ( $p=1.00$ ). This is due to the  
266 biased weighting of linearised PSO kinetics towards data at later times, with the slope of  $\frac{t}{q_e}$  versus  $t$   
267 increasing as equilibrium adsorption is approached, returning smaller values of  $q_e$  and thus giving a  
268 smaller initial rate. The difference between initial rates calculated using linearised and non-linear  
269 PSO kinetics was observed despite equilibrium adsorption kinetic data from the original literature  
270 being excluded in our calculations.

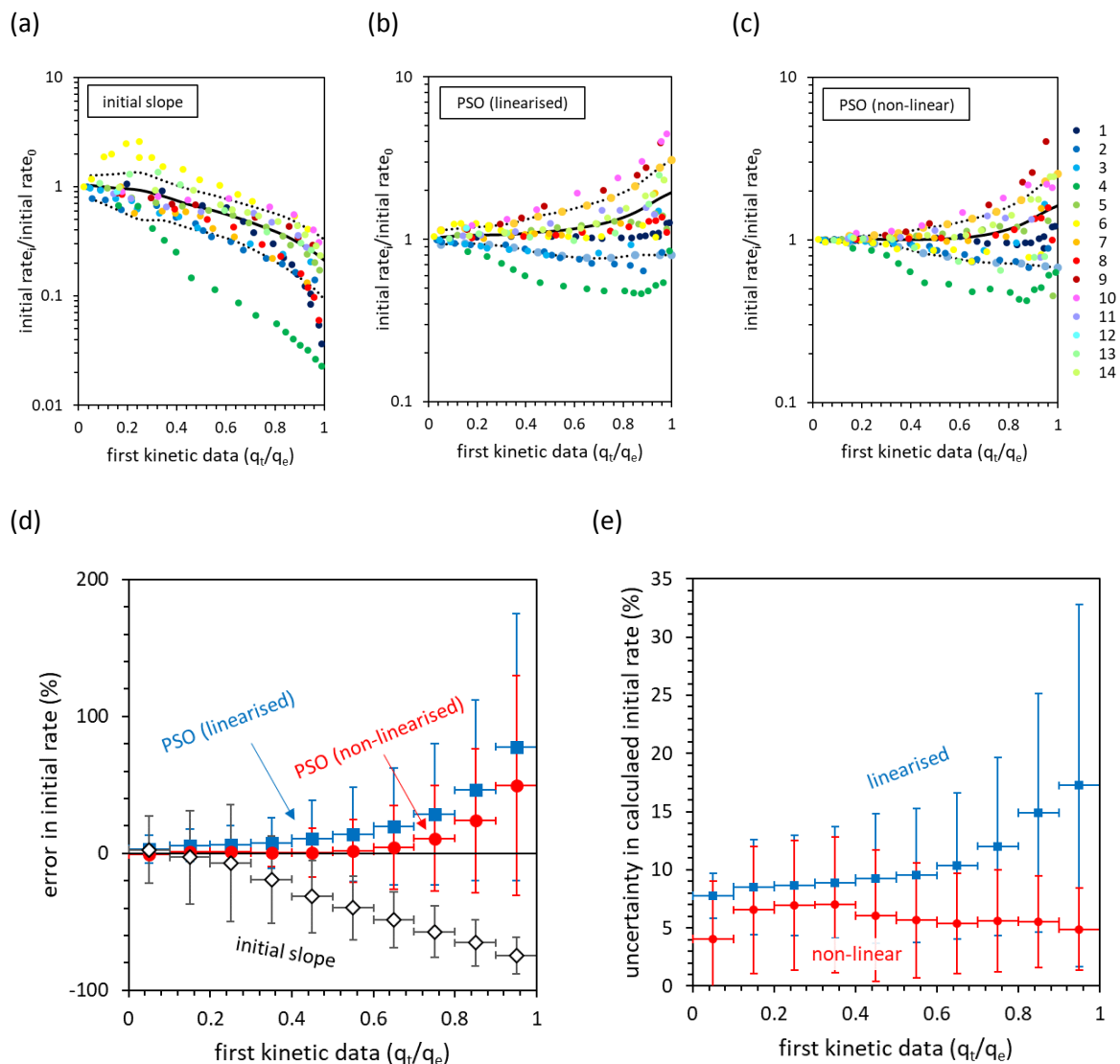
271 Finally, we considered the uncertainties in the initial rates calculated using the two PSO approaches  
272 with varying availability of early kinetic data (Figure 1e). The uncertainties in the initial rates  
273 calculated using linearised PSO kinetics were calculated from the standard error in the linear  
274 regression fit to  $\frac{t}{q_t}$  versus  $t$ , whilst the uncertainties in non-linear PSO kinetics were calculated using  
275 synthetic data and 200 Monte-Carlo simulations<sup>21</sup>. Using linearised PSO kinetics, the propagated  
276 uncertainty in the initial rate increases exponentially as early kinetic data is removed. This is  
277 explained by how late stage adsorption kinetic data is weighted too heavily when fitting linearised  
278 PSO kinetics<sup>10</sup>, where the differences in  $q_t$  are smaller relative to the measurement uncertainty: this  
279 increases the uncertainty of the linear regression. At  $\frac{q_t}{q_e} = 0.6$ , the average uncertainty in the initial  
280 rates calculated using linearised PSO kinetics is 9.5%. In contrast, the uncertainty in the initial rates  
281 calculated using non-linear PSO kinetics is essentially independent of the availability of early kinetic  
282 data, and at  $\frac{q_t}{q_e} = 0.6$  the average uncertainty is only 5.7%.

283 As highlighted here, ideally the data sets used to explore the influence of experimental parameters  
284 such as the adsorbate concentration ( $C_0$ ) and the adsorbent concentration ( $C_s$ ) should include early  
285 kinetic data to reduce the uncertainty in the calculated initial rates. However, literature data  
286 reporting early adsorption kinetics is limited. To provide a balance between the accuracy of our  
287 initial rate calculations and the collection of a sufficient quantity of data sets for statistical analysis,  
288 we set the criterion that data sets must include kinetic data with  $\frac{q_t}{q_e} < 0.6$ . This boundary condition  
289 gives an average error in the calculated initial rate of  $-44 \pm 22$  % for the initial slope approach,  $+17$   
290  $\pm 38$  % using linearised PSO kinetics, and only  $+3 \pm 27$  % for the non-linear PSO kinetics. The results  
291 indicate that non-linear PSO kinetics are most appropriate for calculating initial rates, with an  
292 insignificant systematic error. A  $\sim 30$  % uncertainty remains, associated with how closely the  
293 adsorption kinetics fit to the PSO form (with deviations being both due to inaccurate measurements  
294 and real chemical mechanisms).

295 By considering a literature source reporting two kinetic experiments only, with a different value of  $C_0$   
 296 or  $C_s$  in each, a 30% error in the initial rate of the first experiment (as per the boundary condition of  
 297  $\frac{q_t}{q_e} < 0.6$ ) will confer an error of  $<0.5$  in the calculated reaction order. In this work, the average value  
 298 of  $\frac{q_t}{q_e}$  in the first available kinetic data was 0.37 for experiments where  $C_0$  is varied, and 0.27 for  
 299 experiments where  $C_s$  is varied. Furthermore, the number of kinetic experiments in each literature  
 300 data set was 3-6, indicating that the uncertainties in the calculated initial rates will be  $<30\%$ . Under  
 301 these conditions, the calculated orders of reaction will be accurate to the nearest integer value. This  
 302 was deemed appropriate for the purposes of developing the revised PSO model, given that it is  
 303 common practice for kinetic adsorption models to use integer values for reaction orders (e.g. the  
 304 original PSO equation, and the pseudo-first order kinetic model<sup>9</sup>). In principle, however a similar  
 305 analysis could be made relaxing this condition.

306 Consequently, non-linear fitting of the PSO model was used to determine the initial rate of  
 307 adsorption in each kinetic experiment in all subsequent work.

308



309 *Figure 1: The influence of the limited availability of early kinetic data on the calculation of initial rates of adsorption,*  
310 *assessed by the analysis of 14 literature sources. The influence of removing early kinetic data on the calculated initial rates*  
311 *was assessed using (a) the initial slope, (b) linearised PSO kinetics, and (c) non-linear PSO kinetics. The theoretical 'true'*  
312 *initial rate is given by initial rate<sub>0</sub> and the initial rate calculated with the available data given by initial rate<sub>c</sub>. The solid black*  
313 *line represents the average of the 14 data sets, whilst dotted lines indicate one standard deviation. The three approaches*  
314 *are compared, assessing the influence of data availability on (d) the relative error in the initial rate, and (e) the uncertainty*  
315 *in the calculated initial rate. The horizontal error bars in (d) and (e) represent the size of the bins used for grouping data,*  
316 *whilst the vertical error bars indicate the standard deviation calculated between the 14 unique data sets. The data sets*  
317 *listed are in order: (1) Yang et al., 2019<sup>23</sup>, (2) Yang et al., 2001<sup>24</sup>, (3 and 4) Liu and Shen, 2008<sup>25</sup>, (5) Zhu et al. 2016<sup>26</sup>, (6)*  
318 *Yang et al. 2019<sup>27</sup>, (7) Yang et al. 2019<sup>28</sup>, (8) Mohamed et al. 2007<sup>29</sup>, (9) Drenkova-tuhtan et al. 2015<sup>30</sup>, (10) Liu et al.*  
319 *2016<sup>31</sup>, (11) Ornek et al. 2007<sup>32</sup>, (12) Zhan et al. 2018<sup>33</sup>, (13) Ai et al. 2020<sup>34</sup>, (14) Nadiye-tabbiruka and Sejie 2019<sup>35</sup>.*

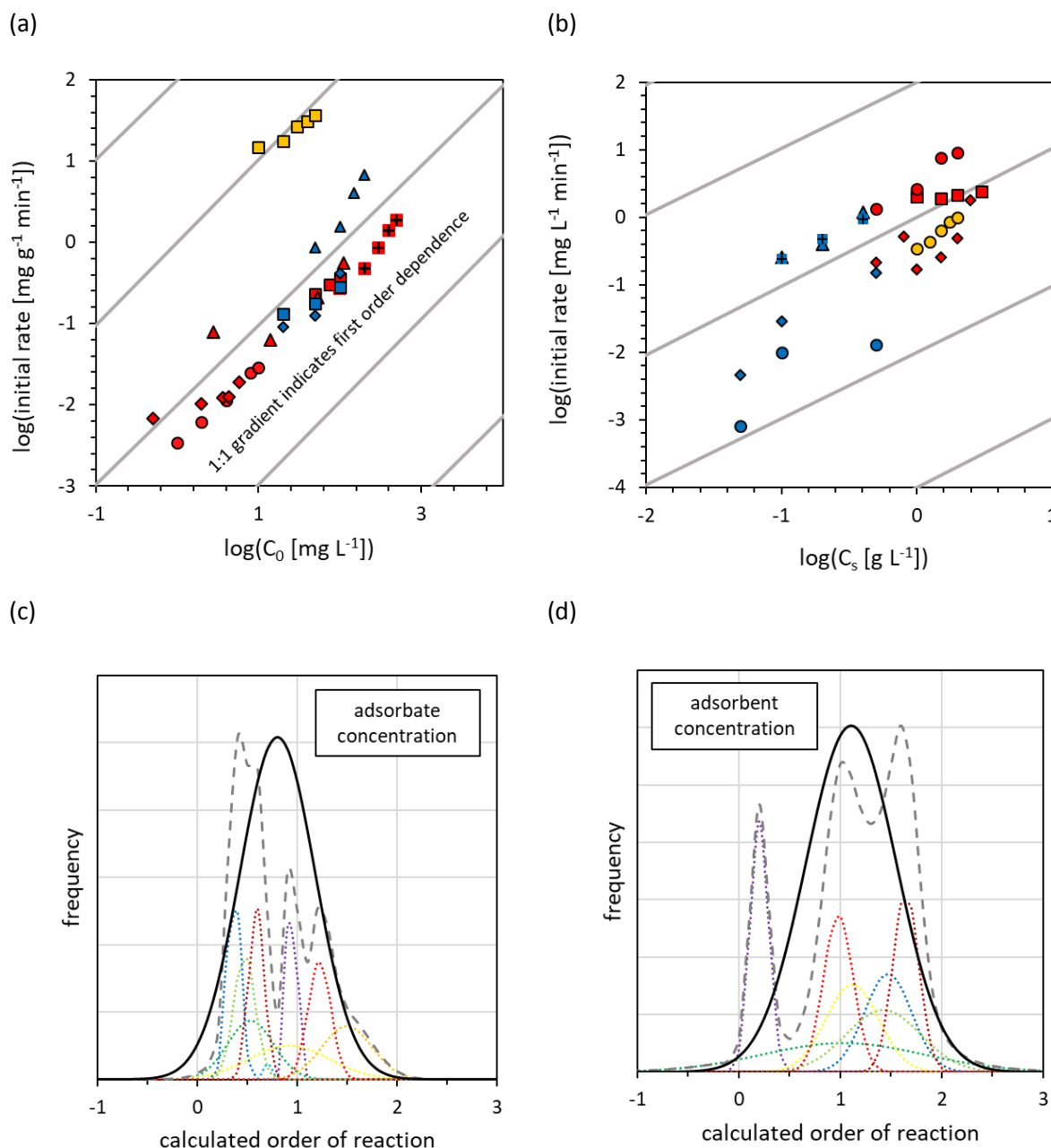
320

### 321 **Determining the influence of $C_0$ and $C_s$ upon the rate of adsorption and the PSO** 322 **rate constant $k_2$**

323 The influence of  $C_0$  and  $C_s$  upon the initial rate of adsorption (calculated as the rate at  $t=0$  using non-  
324 linear PSO kinetics) is presented in Figure 2. For each data set, the order of reaction was determined  
325 from the slope of  $\log(\text{initial rate})$  versus  $\log(C_0)$  or  $\log(C_s)$  (Figure 2a,b). Based upon the evaluation of  
326 uncertainties in the initial rates calculated using non-linear PSO kinetics (in the previous section), the  
327 reaction orders are accurate to the nearest integer value. The data sets tend to show a first-order  
328 dependency of initial rate upon the initial adsorbate concentration ( $C_0$ ) (Figure 2c), with an average  
329 dependency and standard deviation of  $0.80 \pm 0.38$ , and a median value of 0.67. Of the 9 data sets, 7  
330 were closest to first-order dependency, and 2 were closer to zero-order dependency. The sum of  
331 normal distributions representing the reaction orders and uncertainties calculated for each data set  
332 was approximated by a single normal distribution. (However, a larger number of data sets are  
333 needed to verify this). Based upon the standard deviation and assuming a normal distribution in the  
334 results, the relationship between the initial rate and  $C_0$  is first-order with a 90% confidence interval  
335 (1.65 standard deviations). This is intuitive for both diffusion and adsorption-controlled mechanisms,  
336 as twice as much adsorbate should lead to twice as much adsorbate flux from adsorbent surface into  
337 pores, and collisions with the adsorbent surface should be twice as frequent<sup>36,9</sup>.

338 A first-order dependency of initial rates (normalised to  $\text{mg L}^{-1} \text{min}^{-1}$ ) with respect to the adsorbent  
339 concentration ( $C_s$ ) is also observed (Figure 2d), albeit with a wider distribution of results: an average  
340 value of  $1.11 \pm 0.33$  and a median of 1.07. Of the 8 data sets, 6 were closest to first-order  
341 dependency, with 1 data set closer to zero-order and another closer to second-order. Based upon  
342 the standard deviation and assuming a normal distribution in the results, the relationship between  
343 the initial rate and  $C_s$  is also first-order with a 90% confidence interval (1.65 standard deviations).  
344 This is again intuitive for both diffusion and adsorption-controlled mechanisms, as when  $C_s$  is  
345 doubled the total surface area available to solution ( $\text{m}^2 \text{L}^{-1}$ ) is doubled, the overall flux of adsorbate  
346 entering adsorbent pores is doubled, and the rate of collisions between adsorbate and total  
347 adsorbent surface is also doubled. When normalised to mass ( $\text{mg g}^{-1} \text{min}^{-1}$ ) the initial rate is zero-  
348 order with respect to  $C_s$ , as expected.

349

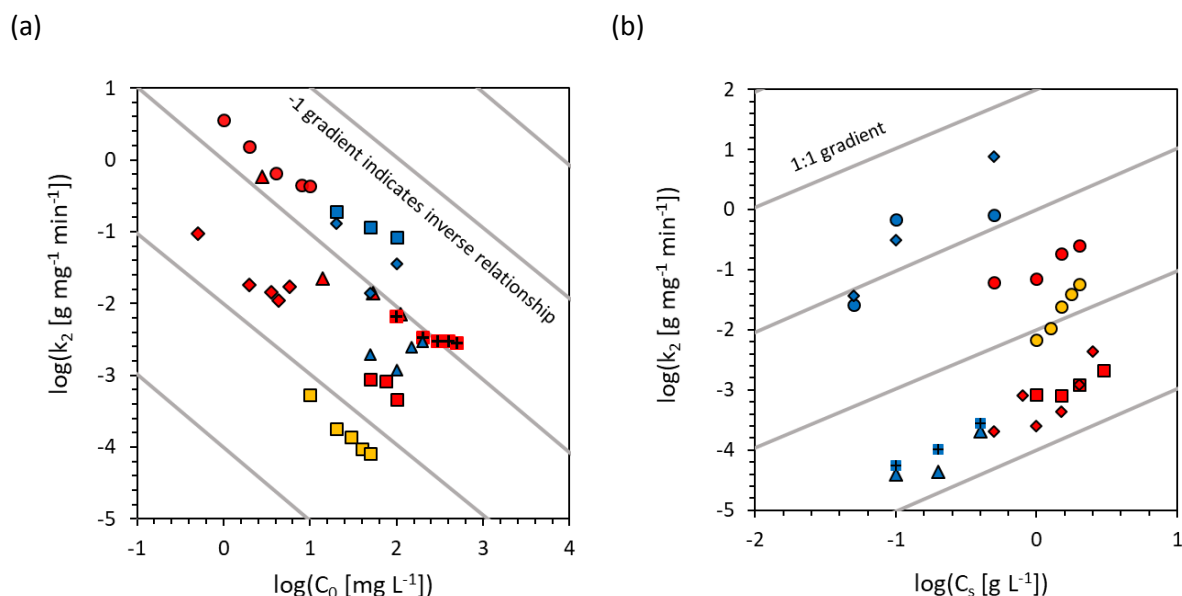


350 *Figure 2: Determining the influence of initial adsorbate concentration ( $C_0$ ) and adsorbent concentration ( $C_s$ ) on the initial*  
 351 *rate of adsorption using literature data sets. The order of reaction was determined from the slope of  $\log(\text{initial rate})$  as a*  
 352 *function of (a)  $\log(C_0)$  and (b)  $\log(C_s)$ , with each data point representing a single kinetic experiment (with unique values of  $C_0$*   
 353 *and  $C_s$ ). All experiments in a given data set (one literature paper, where all experimental conditions except for either  $C_0$  or  $C_s$*   
 354 *are constant) are grouped by colour and symbol, with oxyanions in red, metal cations in blue, and organic dyes in yellow (a*  
 355 *legend referencing the literature sources is presented in SI Figure S2). Uncertainties were calculated from the standard error*  
 356 *in the slope. The results are alternatively presented using normal distributions with the mean given by the slope and the*  
 357 *standard deviation given by the standard error of the slope (c and d). Here, each data set is represented by a dotted line,*  
 358 *and the sum of all data sets given by the dashed line. Solid black lines represent the normal distribution obtained by the*  
 359 *average of all data sets.*

360

361 For both predictive modelling and the comparison of adsorption kinetics between literature sources,  
 362 it is necessary that rate constants are not affected by the experimental conditions. Whilst adsorption  
 363 kinetics are typically first-order with respect to  $C_0$ , the PSO rate constant  $k_2$  is inversely proportional

364 to  $C_0$  (Figure 3a). Consequently, whilst doubling the initial adsorbate concentration typically  
 365 increases the initial rate of adsorption by a factor of two, counter-intuitively the PSO rate constant  $k_2$   
 366 will decrease by a factor of two. The average slope of  $\log(k_2)$  versus  $\log(C_0)$  is  $-0.73 \pm 0.46$ . The inverse  
 367 relationship between  $k_2$  and  $C_0$  is explained by the second-order dependence of the PSO model upon  
 368 the **absolute** concentration of available adsorption capacity remaining through the term  $(q_e - q_t)^2$ . In  
 369 cases where the adsorbent is unsaturated, increasing  $C_0$  by a factor of two will approximately double  
 370  $q_e$ . The parameter  $(q_e - q_t)^2$  at  $t=0$  will increase by a factor of four, and consequently  $k_2$  must decrease  
 371 by a factor of two to achieve the observed doubling of initial rates.



372 *Figure 3: Dependence of the pseudo-second order (PSO) rate constant  $k_2$  upon (a) initial adsorbate concentration ( $C_0$ ), and*  
 373 *(b) adsorbent concentration ( $C_s$ ). The data is presented as described in Figure 2, with a legend referencing the literature*  
 374 *sources presented in SI Figure S2.*

375

376 In contrast, a positive relationship between  $C_s$  and  $k_2$  is observed, with an average dependency of  
 377  $1.57 \pm 0.85$  (Figure 3b). (First and second-order dependencies between  $k_2$  and  $C_s$  are both included  
 378 within the standard deviation). This is explained by how when  $C_s$  is doubled,  $q_e$  will decrease by a  
 379 factor of between 0 and 2: zero when the adsorbate is in excess and  $q_e$  is insignificant compared to  
 380  $C_0$ , and two when the adsorbent is in excess and  $q_e$  is large relative to  $C_0$ . Consequently, as  $C_s$   
 381 increases,  $(q_e - q_t)^2$  decreases with a zero-to-second-order dependency, and to achieve the zero-order  
 382 relationship between  $C_0$  and initial rates ( $\text{mg g}^{-1} \text{min}^{-1}$ ),  $k_2$  must also increase with a dependency that  
 383 is between zero and second-order.

384

385 **Revision of the pseudo-second order (PSO) rate equation to account for**  
 386 **changes in adsorbate ( $C_0$ ) and adsorbent ( $C_s$ ) concentrations**

387

388 **Modification of the PSO rate equation**

389 In this section, we modify the original PSO rate equation to include the appropriate sensitivity  
 390 towards  $C_0$  and  $C_s$ , meeting the aims of (a) improving the predictive capacity of this model, and (b)  
 391 normalising rate constants for better comparison across the literature.

392 Firstly, for a given concentration of adsorbent, the total concentration of adsorption surface sites is  
 393 constant regardless of the value of  $C_0$ . The term within the rate equation used to represent the  
 394 contribution of adsorption surface site availability towards the rate of reaction should therefore be  
 395 independent of  $C_0$ . The original PSO rate equation contains a second-order dependence upon the  
 396 **absolute amount** of adsorption capacity remaining,  $(q_e - q_t)^2$ , which gives the undesirable inverse  
 397 relationship between the rate constant and  $C_0$  demonstrated in Figure 3a. This term can be replaced  
 398 with a second-order dependence upon the **relative amount** of adsorption capacity remaining,  
 399  $\left(1 - \frac{q_t}{q_e}\right)^2$ , which will always return a value of 1 at time  $t=0$ , independent of  $C_0$ . This term therefore  
 400 describes the contribution of adsorption surface site availability towards the rate of adsorption more  
 401 appropriately than the original PSO term  $(q_e - q_t)^2$ . Here,  $\frac{q_t}{q_e}$  is the same as the parameter  $\theta$  used in the  
 402 Langmuir adsorption isotherm model<sup>20</sup>. This modification of Equation 1 gives the following:

403 
$$\frac{dq_t}{dt} = k'' \left(1 - \frac{q_t}{q_e}\right)^2$$

404 Equation 10

405 where  $k'' = k_2 q_e^2$ .

406 The first-order dependence of the reaction rate upon the adsorbate concentration observed  
 407 experimentally (Figure 2c) is then defined within the rate equation, giving:

$$\frac{dq_t}{dt} = k' C_t \left(1 - \frac{q_t}{q_e}\right)^2$$

408 Equation 11

409 where  $k' = \frac{k_2 q_e^2}{C_0}$ . The rate constant  $k'$  takes the units  $L g^{-1} min^{-1}$ .

410 The initial rate of adsorption tends to be zero-order with respect to  $C_s$  (when normalised to  
 411 adsorbent mass with the units  $mg g^{-1} min^{-1}$ ). The original PSO model gives an initial rate that varies  
 412 with changes in  $C_s$ , due to its second-order dependence upon the absolute adsorption capacity  
 413 remaining  $(q_e - q_t)^2$  and the decrease in  $q_e$  with increasing  $C_s$ . In contrast, since the rPSO depends on  
 414 the relative adsorption capacity remaining through the term  $\left(1 - \frac{q_t}{q_e}\right)^2$ , this rate equation displays  
 415 the zero-order dependency of  $C_s$  identified from analysis of the literature. The rPSO rate constant  $k'$   
 416 is therefore theoretically independent of changes in  $C_s$ , unlike the original PSO rate constant  $k_2$ . The



417 rPSO model is similar to the adsorption-only form of the kinetic Langmuir model (kLm), which at high  
418 surface coverage is first order with respect to  $C_t$  and second order to  $(1 - \frac{q_t}{q_e})^{37, 38}$ .

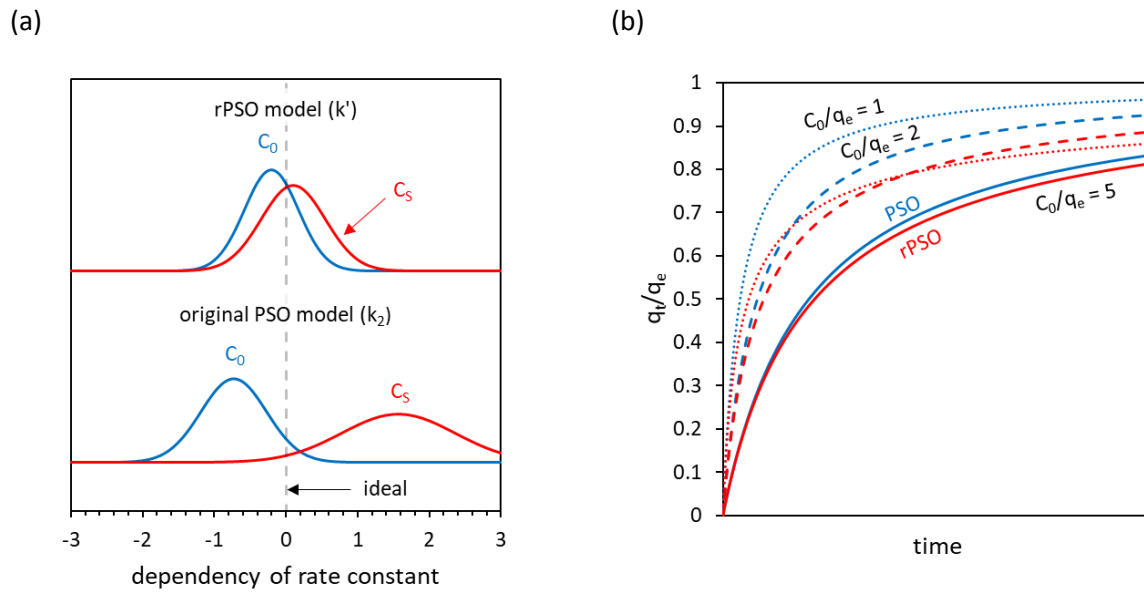
419

#### 420 **Validation of the rPSO rate equation**

421 The removal of experimental conditionality (i.e. the dependency upon  $C_0$  and  $C_s$ ) from the revised  
422 model was verified using experimental data from the literature. The ideal rate constant is unaffected  
423 by the experimental conditions, and subsequently the dependency of the rate constant with respect  
424 to  $C_0$  and  $C_s$  should be zero. These dependencies were calculated from the slope of log(rate  
425 constant) versus log( $C_0$ ) or log( $C_s$ ). As highlighted by Figure 4a, the original PSO rate constant  $k_2$  is  
426 strongly dependent upon the experimental conditions, being inversely proportional to  $C_0$  and  
427 second-order with respect to  $C_s$ . The average  $C_0$  dependency is  $-0.73 \pm 0.46$ , and the average  $C_s$   
428 dependency is  $1.57 \pm 0.79$ . In contrast,  $k'$  is approximately zero-order with respect to both  
429 experimental variables. Furthermore, the dependencies of  $k'$  upon  $C_0$  and  $C_s$  vary less (there is less  
430 scattering) than  $k_2$ . The average  $C_0$  dependency is  $-0.20 \pm 0.38$  and the average  $C_s$  dependency is  
431  $0.10 \pm 0.45$ . These results demonstrate that the new rate constant  $k'$  is less conditional than  $k_2$ , and  
432 that the dependency of adsorption kinetics upon  $C_0$  and  $C_s$  is captured by the new model.

433 When the adsorbate is in excess ( $q_e < C_0$ ) the rPSO model approximates the form of the original PSO  
434 model. At higher values of  $q_e$  relative to  $C_0$ , the graphical form of the two models deviates, due to  
435 the rPSO kinetics decreasing more rapidly than PSO kinetics due to the consumption of the  
436 adsorption, which decreases the parameter  $C_t$ . (However, this effect is logical, given that at low  $C_t$   
437 values, the rate of adsorption will be limited by the availability of adsorbate). Therefore, rate  
438 constants for the rPSO ( $k'$ ) can be readily calculated from PSO parameters  $k_2$  and  $q_e$  when the  
439 adsorbate is in excess, using the formula  $k' = \frac{k_2 q_e^2}{C_0}$ . When the adsorbent removes the majority of  
440 the adsorbate, however, the rPSO model will require re-fitting due to the increasing difference in the  
441 graphical form of the PSO and rPSO models.

442



443 Figure 4: Verifying that experimental conditionality (with respect to  $C_0$  and  $C_s$ ) is decreased in the rPSO model versus the  
 444 original PSO model. (a) The dependencies of the original PSO rate constant  $k_2$  and the rPSO rate constant  $k'$  upon  $C_0$  and  $C_s$   
 445 were calculated from the slope of log plots, as per Figure 3, with the ideal rate constant giving a reaction order or  
 446 'dependency' of zero. The data is shown as normal distributions with the mean and standard deviation set equal to the  
 447 slope and standard error of the slope in the log plots (with 9 data sets for  $C_0$  and 8 for  $C_s$ ). These values are:  $-0.73 \pm 0.46$  for  
 448  $k_2$  and  $C_0$ ;  $1.57 \pm 0.79$  for  $k_2$  and  $C_s$ ;  $-0.20 \pm 0.38$  for  $k'$  and  $C_0$ ;  $0.10 \pm 0.45$  for  $k'$  and  $C_s$ . (b) A comparison of the form of the  
 449 original PSO equation with the rPSO equation, with different  $\frac{C_0}{q_e}$  ratios (with  $C_s = 1 \text{ g L}^{-1}$ ). The original PSO model is presented  
 450 in blue and the rPSO model in red, with  $\frac{C_0}{q_e}$  equal to 1 (dotted lines), 2 (dashed lines), and 5 (solid lines).

451

452

### Example applications

453

454

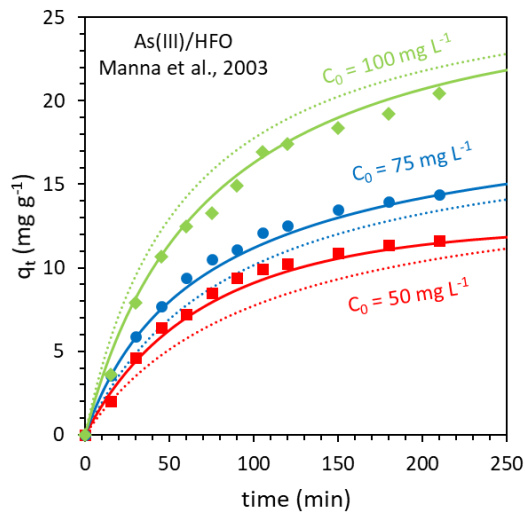
#### Application 1: Evaluating the predictive capability of the revised PSO model

455 The first objective of this work was to provide a simple modification of the popular PSO model to  
 456 introduce predictive capabilities, for the purpose of engineering studies<sup>39</sup>. If the kinetic model is to  
 457 be used to predict adsorption performance under different conditions, then it is essential that the  
 458 model parameters obtained experimentally are valid in a range of scenarios. Consequently, we  
 459 evaluated whether the rPSO model would provide a better fit to experimental data compared  
 460 against the PSO model, if a single rate constant is used to model multiple experiments with different  
 461 values of  $C_0$  and  $C_s$ .

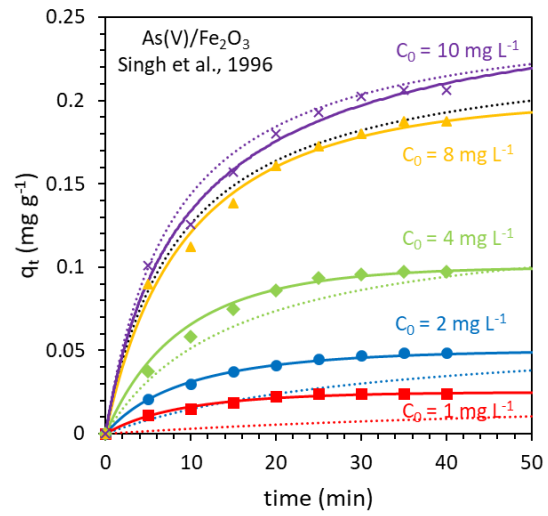
462 The original PSO model tends to systematically overestimate  $q_t$  for experiments with high  $C_0$  or low  
 463  $C_s$  values and systematically underestimate  $q_t$  for experiments with low  $C_0$  or high  $C_s$  values (Figure  
 464 5). This is due to the negative and positive relationships between  $k_2$  and  $C_0$  and  $C_s$  respectively as  
 465 previously discussed, with this relationship being denied when a single value of  $k_2$  is used to model  
 466 all experiments. The rPSO model gave a better fit to experimental data (i.e. a smaller sum of squared  
 467 residuals) in 5 of the 6 data sets tested (all panels in Figure 5 except d) and the median decrease in  
 468 the sum of squared residuals when changing from the PSO to the rPSO model was 66%.

469

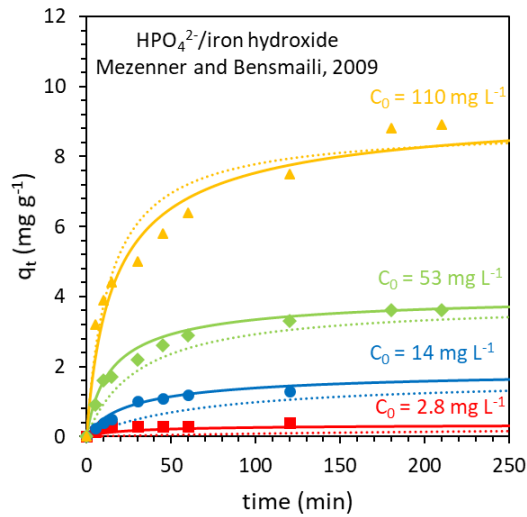
(a)



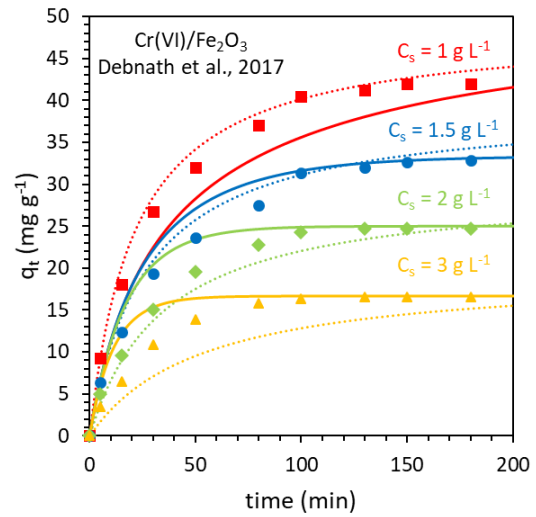
(b)



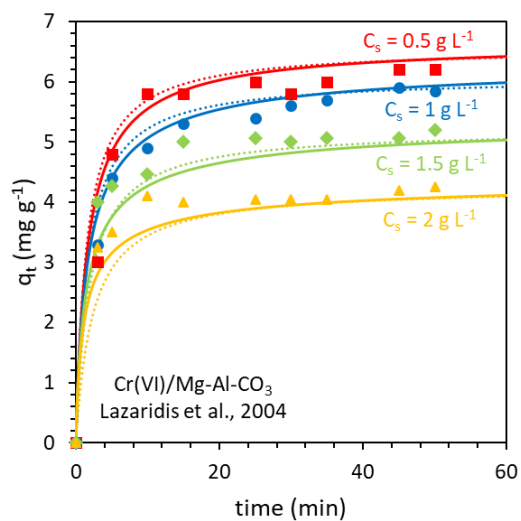
(c)



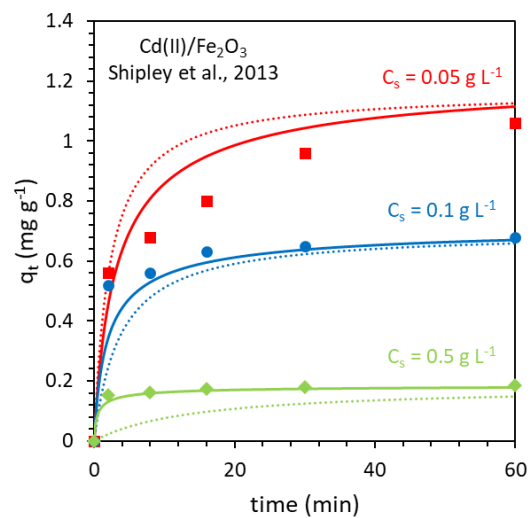
(d)



(e)



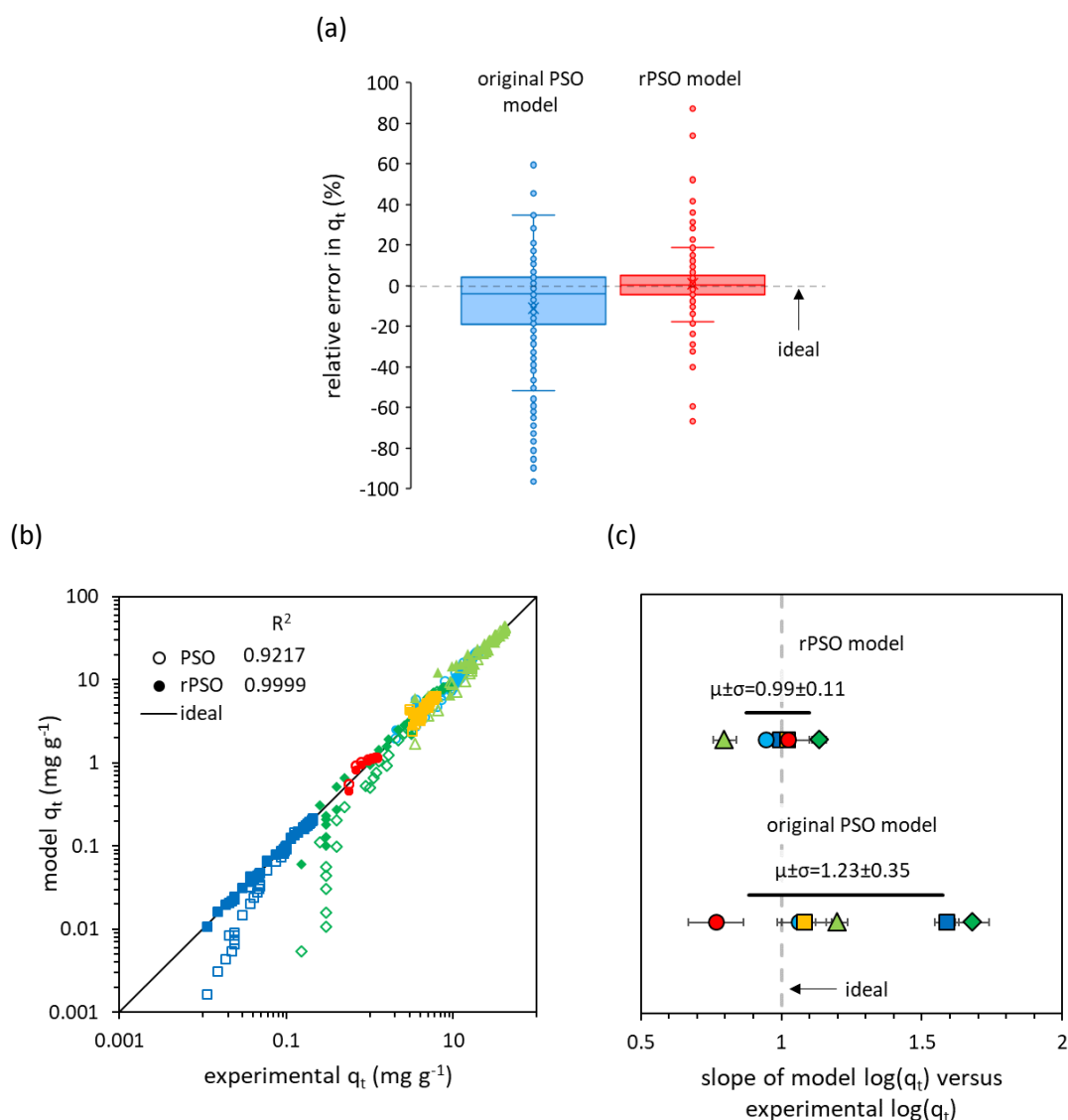
(f)



470 Figure 5: Application study 1: Application of the revised PSO (rPSO) model (solid lines) to describe multiple experiments with  
 471 a single rate constant, compared against the original PSO model (dotted lines). (a,b,c) present 3 experiments where  $C_0$  is  
 472 varied, and (d,e,f) present 3 experiments where  $C_s$  is varied. Experimental data was sourced from Manna et al. (2003)<sup>40</sup>,  
 473 Singh et al. (1996)<sup>41</sup>, Mezenner and Bensmaili (2009)<sup>42</sup>, Debnath et al. (2017)<sup>43</sup>, Lazaridis et al. (2004)<sup>44</sup>, and Shipley et al.  
 474 (2013)<sup>45</sup>.

475

476 The average relative error of  $q_t$  calculated by the rPSO is just  $1\pm 17\%$ , versus  $-11\pm 27\%$  for the original  
 477 PSO model (Figure 6a), indicating that the rPSO model provides greater accuracy when modelling  
 478 adsorption kinetics with changing values of  $C_0$  and  $C_s$  using a single rate constant. Furthermore, the  
 479 calibration curve of  $q_t$  (model) against  $q_t$  (experiment) is closer to the ideal one-to-one line in the  
 480 rPSO model, with an  $R^2$  value of 0.999 versus just 0.9217 for the original PSO model (Figure 6b).  
 481 Considering each experimental data series in turn, the typical slope of the calibration curve was  
 482 closer to one, with less scattering, in the rPSO model (a slope of  $0.99\pm 0.11$ ) compared against the  
 483 original PSO model (with a slope of  $1.23\pm 0.35$ ) (Figure 6c).



484 Figure 6: Application study 1: Cross-calibration of the rPSO model against experimental data (6 literature sources, 22  
 485 experiments and 198 data points). (a) Box and whisker plot presenting the relative error of  $q_t$  calculated via the original PSO  
 486 model and the rPSO model. The boxes highlight the 25%, 50% (median) and 75% percentiles, whilst the whiskers represent

487 the minima and maxima excluding 'outlier' data points, defined as those greater than the top of the box plus 1.5 times the  
488 interquartile range, or less than the bottom of the box minus 1.5 times the interquartile range. (b) Cross-calibration plot  
489 highlighting the goodness of fit against the one-to-one line. Open shapes indicate  $q_t$  values calculated using the original PSO  
490 model, whilst filled shapes indicate the rPSO model. Values of  $R^2$  indicate the goodness of fit against the ideal one-to-one  
491 line. (c) Comparison of the cross-calibration slopes with each model and each data set. Literature sources are denoted as  
492 As(III)/HFO<sup>40</sup> (dark blue squares), As(V)/Fe<sub>2</sub>O<sub>3</sub><sup>41</sup> (light blue circles), HPO<sub>4</sub><sup>2-</sup>/iron hydroxide<sup>42</sup> (dark green diamonds),  
493 Cr(VI)/Fe<sub>2</sub>O<sub>3</sub><sup>43</sup> (light green triangles), Cr(VI)/Mg-Al-CO<sub>3</sub><sup>44</sup> (orange squares), and Cd(II)/Fe<sub>2</sub>O<sub>3</sub><sup>45</sup> (red circles). Further results  
494 are presented in SI Figure S3.

495

496 Whilst the rPSO rate constant  $k'$  appears to be more stable to changes in experimental conditions  
497 than the PSO rate constant  $k_2$ , the parameter  $q_e$  is conditional, depending upon  $C_0$  and  $C_s$ . For  
498 predictive modelling, this limitation can be rectified by using an adsorption isotherm to predict  $q_e$   
499 (such as the Langmuir or Freundlich model<sup>46</sup>). Though a single value of  $q_e$  can be determined for the  
500 entirety of each experiment, in scenarios such as a column reactor the equilibrium adsorbate  
501 concentration parameter  $C_e$  has diminished physical significance, and it may be better to replace this  
502 term with  $C_t$ , recalculating the hypothetical value of  $q_e$  at each point in time. Huang et al. previously  
503 demonstrated that this approach can give a better account of the true driving force of the reaction  
504 during the initial stages of adsorption<sup>47</sup>.

505

## 506 **Application 2: Comparison of rate constants between different experimental studies**

507 Comparison of the rPSO rate constant  $k'$  is expected to be more meaningful and more appropriate  
508 than  $k_2$  when comparing the adsorption kinetics reported in the literature using different  
509 experimental conditions, since some of the experimental conditionality (towards changes in  $C_0$  and  
510  $C_s$ ) is accounted for. To demonstrate the potential application of normalised rate constants towards  
511 achieving a meaningful comparison of the adsorption kinetics reported across the literature, we  
512 collected 14 and 7 literature sources reporting the kinetics of inorganic arsenic As(V) and As(III)  
513 adsorption onto iron oxide and alumina adsorbents respectively.

514 The average value of  $\log(k_2)$  for all iron oxide studies is  $-0.93 \pm 1.50$ , whilst the average of  $\log(k')$  is -  
515  $1.05 \pm 1.08$ . In both cases, the standard deviation is large, with more than an order of magnitude  
516 variation in  $k_2$  and  $k'$  values: neither model provides a rate constant that is generally valid for iron  
517 oxide adsorbents used by different studies. Similarly, the adsorption of inorganic arsenic onto  
518 alumina gives average values of  $\log(k_2) = 0.98 \pm 1.84$  and  $\log(k') = 0.35 \pm 1.75$ .

519 Whilst the variation in both  $k_2$  and  $k'$  across the literature is large, the influence of adsorbent  
520 morphology on adsorption kinetics has not been incorporated into either of the PSO and rPSO  
521 models. Adsorption kinetics are often faster for adsorbent materials with smaller particles, due to  
522 the improved rate of mass transport of the adsorbate to adsorbent surface sites<sup>48</sup>. For instance, in  
523 intraparticle diffusion model gives a rate of adsorption that is proportional to  $r^{-1}$  (where  $r$  is particle  
524 size)<sup>49</sup>.

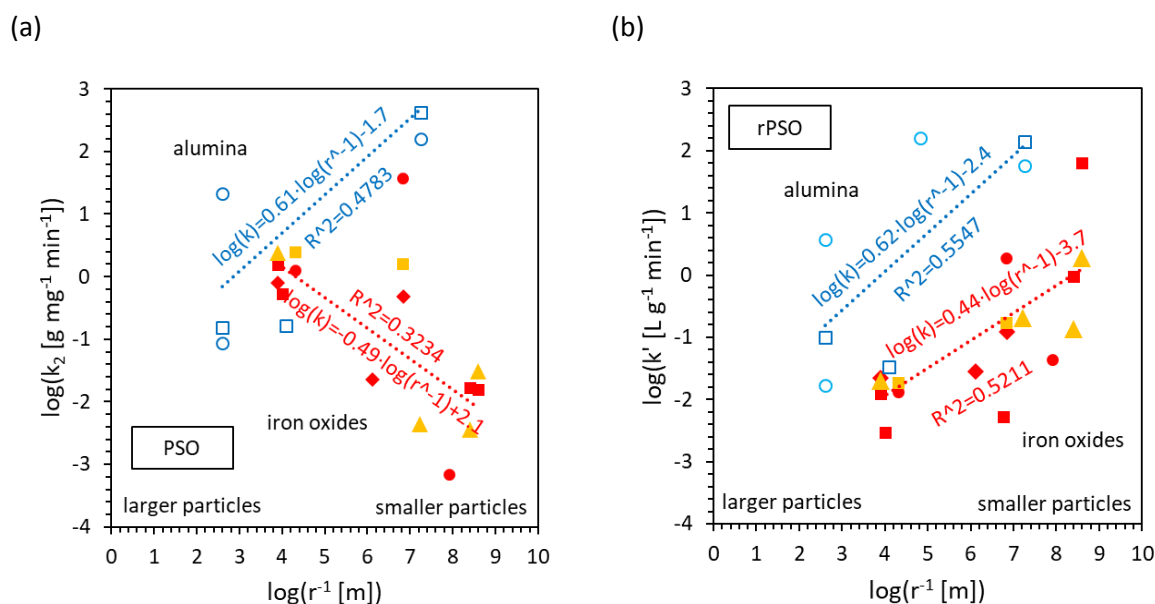
525 Whilst a faster reaction is anticipated for small iron oxide particle sizes, plotting  $\log(k_2)$  as a function  
526 of  $\log(r^{-1})$  shows a weak inverse relationship (linear regression gives a slope of  $-0.49 \pm 0.20$  and  
527  $R^2 = 0.3234$ ) (Figure 7a). This is due to the significant increase in  $q_e$  as the particle size decreases (SI  
528 Figure S4) and the inverse relationship between  $k_2$  and  $q_e$  through the term  $(q_e - q_t)^2$  as previously

529 discussed. In contrast, alumina shows the anticipated positive relationship (with a slope of  $0.61 \pm 0.28$   
 530 and  $R^2=0.4783$ ). Since adsorption onto smaller particles is typically faster than onto larger particles,  
 531 the comparison of  $k_2$  values for different adsorbent sizes and different adsorbent materials (i.e. iron  
 532 oxides versus alumina) is not useful and is likely to lead to false conclusions.

533 In contrast, we see the anticipated positive relationship for  $\log(k')$  as a function of  $\log(r^{-1})$  for both  
 534 iron oxide and alumina adsorbents (Figure 7b). For the iron oxides we see a slope of  $0.44 \pm 0.1$  with  
 535  $R^2=0.5211$ , and for alumina we see a slope of  $0.62 \pm 0.25$  and  $R^2=0.5547$ . The limited goodness of fit in  
 536 the linear regression is controlled by factors including poor characterisation of the particle size and  
 537 differences in experimental conditions beyond  $C_0$  and  $C_s$ , such as the pH. The accurate  
 538 characterisation of particle size is especially challenging, given the range of techniques used by the  
 539 literature including transmission electron microscopy (TEM), dynamic light scattering (DLS) and sieve  
 540 fractionation.

541 The results from this literature survey show greater values of  $\log(k')$  at each specific particle size for  
 542 alumina versus iron oxides, suggesting that the adsorption of inorganic arsenic is faster onto alumina  
 543 than onto iron oxides. With more rigorous analysis, such a study would have important implications  
 544 in the design of engineered solutions for arsenic remediation, i.e. opting to use alumina in place of  
 545 iron oxides when high flow rates in a column filter are required, or when larger particle sizes are  
 546 necessary to achieve the desired flow rate and porosity. This highlights that normalisation of the PSO  
 547 rate constant  $k_2$  to the rPSO rate constant  $k'$ , or some other constant, can achieve a more  
 548 meaningful comparison of the adsorption kinetics reported by the literature.

549



550 *Figure 7: Application study 2: Use of the rPSO rate constant  $k'$  to compare literature sources with adsorption kinetics*  
 551 *determined under different experimental conditions. Particle size decreases from left to right. Presented are As(V) (red filled*  
 552 *shapes) and As(III) (orange filled shapes) adsorption onto iron oxides, and As(V) (dark blue open squares) and As(III) (light*  
 553 *blue open circles) adsorption onto alumina. Each data point indicates a different literature source, with a legend given in SI*  
 554 *Figure S5.*

## Conclusions

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This work aimed to modify the popular pseudo-second order (PSO) model of adsorption kinetics to remove experimental conditionality, focusing upon initial adsorbate concentration ( $C_0$ ) and adsorbent concentration ( $C_s$ ). A revised PSO rate equation (rPSO) was developed from the empirical analysis of 69 kinetic experiments taken from 15 literature sources. The final equation takes the form  $\frac{dq_t}{dt} = k' C_t (1 - \frac{q_t}{q_e})^2$ . The first application study demonstrates that the rPSO equation allows for a single rate constant to model multiple experiments, differing in the experimental conditions  $C_0$  and  $C_s$ , with greater accuracy and a 66% decrease in the sum of squared residuals versus the original PSO model. The second application study demonstrates that the rPSO equation provides a rate constant which is more useful for comparison across the literature than the PSO rate constant  $k_2$ , obeying the anticipated relationship between adsorption rates and particle size.

The new rate equation is similar to an adsorption-only form of the kinetic Langmuir model (kLm), which at high surface coverage is first order with respect to  $C_t$  and second order with respect to  $(1 - \frac{q_t}{q_e})$ <sup>37 38</sup>. However, the rPSO equation is simpler, with fewer fitting parameters needed, and may thus be more useful for the non-expert. The rPSO equation may prove more useful than the original PSO model in engineering studies where operating conditions are likely to vary.

One of the reasons for the popularity of the original PSO model is its linearised forms, from which  $k_2$  and  $q_e$  parameters can be readily obtained from experimental data. Whilst, we have unfortunately not yet found a way to linearise the rPSO rate equation, it is worth noting that linearisation of the original PSO model often results in a poorer quality of fit versus when using non-linear fitting<sup>14</sup>. Where necessary, the rate constant for this revised model can be quickly obtained from linearised PSO kinetics using the expression  $k' = \frac{k_2 q_e^{\dagger 2}}{C_0^{\dagger}}$ .

In our analytical approach, we demonstrate that non-linear fitting of PSO kinetics is more appropriate than linearised PSO kinetics and the initial slope approach when early kinetic data is limited, as is often the case in adsorption experiments. Our literature survey only yielded 9 data sets where  $C_0$  was varied and 8 where  $C_s$  was varied, satisfying our requirements for early kinetic data with  $\frac{q_t}{q_e} < 0.6$ . This highlights a need for experimental work to investigate the influence of these independent variables more systematically, and to ensure that initial adsorption kinetics are adequately captured, given that the method of initial rates is typically considered the superior approach towards determining reaction orders<sup>17</sup>.

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592        **Supporting information**

593        The supplementary information provides references to all data sets used in this work; figures  
594        showing the influence of adsorbent morphology on  $k_2$ ; and tabulates all parameters ( $q_e$ ,  $k_2$ ,  $k'$  and  
595        initial rate) calculated in this work.

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